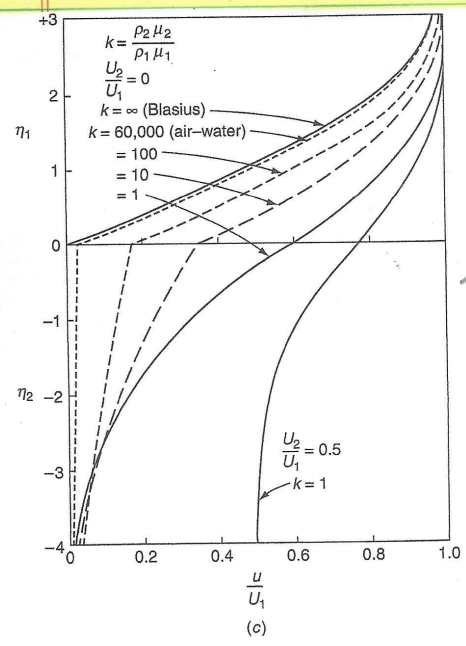


2D mixing layer: free shear layer

Two parallel streams, U_1 (upper) & U_2 (lower) meet at $x=0$. Progression downstream smoother discontinuity due to μ into S shaped velocity profile is free-shear layer.

Assume $p = \text{constant}$ upper/lower layer is $p_x = 0$ such that $y=0$ dividing x at BL assumptions is same idea as flat plate BL but with different BC. Therefore use Blasius type similarity variable $\eta = \left(\frac{u_1}{\nu_{mix}}\right)^{1/2} \frac{y}{x}$ at $x = \left(\frac{u_1}{\nu_{mix}}\right)^{1/2} f(\eta)$



water at $y=0$
 $\mu_{mix} = \mu_{avg}$
 such that μ itself important physical property not just $\nu = \mu/\rho$

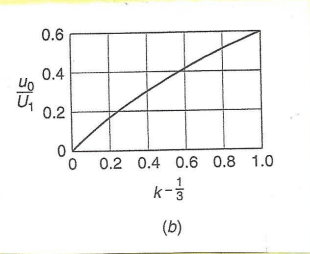
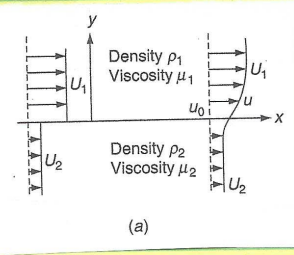


FIGURE 4-17 Velocity distribution between two parallel streams of different properties: (a) geometry; (b) velocities at the interface ($U_2 = 0$) (c) representative velocity profiles. [After Lock (1951).] (By permission of The Clarendon Press, Oxford.)

Blasius Similarity

$$2u u_x + v u_y = \nu u_{yy}$$

$$u_x = u_1 f'_\alpha = \gamma_\alpha y$$

$$\gamma_{\alpha y} = [\nu u_1 x]^{1/2} f'_\alpha \gamma_{\alpha y}$$

$$= [\nu u_1 x]^{1/2} [u_1 / \nu x]^{1/2} f'_\alpha$$

$$= u_1 f'$$

$$\gamma_\alpha = (\nu u_1 x)^{1/2} f'_\alpha (\gamma_\alpha) = g_\alpha(x) f'_\alpha$$

$$\gamma_\alpha = [u_1 / \nu x]^{1/2} y$$

$$= h_\alpha(x) y$$

$$\gamma_{\alpha x} = y h_{\alpha x} = \frac{\gamma_\alpha}{h_\alpha} h_{\alpha x}$$

$$\gamma_{\alpha y} = h_\alpha \quad \gamma_{\alpha \gamma y} = 0$$

$$v_x = -\gamma_{\alpha x} = -\left(g_{\alpha x} f'_\alpha + g_\alpha f''_{\alpha x} \right) = -\left(g_{\alpha x} f'_\alpha + g_\alpha f''_{\alpha x} \gamma_{\alpha x} \right)$$

$$-v_x = \frac{1}{2} \left[\frac{\nu u_1}{x} \right]^{1/2} f'_\alpha + [\nu u_1]^{1/2} x^{-1/2} f''_{\alpha x} \gamma_\alpha (-\frac{1}{2} x^{-1}) \quad g_\alpha(x) = [\nu u_1]^{1/2} x^{1/2}$$

$$g_{\alpha x} = [\nu u_1]^{1/2} \frac{1}{2} x^{-1/2}$$

$$= \frac{1}{2} \left[\frac{\nu u_1}{x} \right]^{1/2}$$

$$v_x = \frac{1}{2} \left[\frac{\nu u_1}{x} \right]^{1/2} [\gamma_\alpha f''_{\alpha x} - f'_\alpha]$$

$$u_{\alpha x} = u_1 f''_{\alpha x} \gamma_{\alpha x} = u_1 f''_{\alpha x} \left(-\frac{\gamma}{2x} \right)$$

$$h_\alpha = \left[\frac{u_1}{\nu x} \right]^{1/2} x^{-1/2}$$

$$u_{\alpha y} = u_1 f''_{\alpha x} \gamma_{\alpha y} = u_1 f''_{\alpha x} [u_1 / \nu x]^{1/2}$$

$$h_{\alpha x} = -\frac{1}{2} \left[\frac{u_1}{\nu x} \right]^{1/2} x^{-3/2}$$

$$u_{\alpha \gamma y} = u_1 f'''_{\alpha x} \gamma_{\alpha y} = u_1 f'''_{\alpha x} [u_1 / \nu x]^{1/2}$$

$$h_{\alpha x} / h_\alpha = -\frac{1}{2} \left[\frac{u_1}{\nu x} \right]^{1/2} x^{-3/2} / \left[\frac{u_1}{\nu x} \right]^{1/2} x^{-1/2}$$

drop

$$u_1 f' [u_1 f'' \left(-\frac{\gamma}{2x} \right)] + \frac{1}{2} \left[\frac{\nu u_1}{x} \right]^{1/2} [\gamma f' - f] u_1 f'' \left[\frac{u_1}{\nu x} \right]^{1/2} = -\frac{1}{2} x^{-1}$$

$$= \nu u_1 f''' [u_1 / \nu x]$$

$$\gamma_{\alpha x} = -\frac{\gamma}{2x}$$

$$2x \left(-\frac{\gamma}{2x} \right) f' f'' + \frac{1}{2} \left(\frac{\nu u_1}{x} \right)^{1/2} [\gamma f' - f] f'' = \frac{\nu u_1}{x} f'''$$

$$-\gamma f' f'' + \frac{1}{2} (\gamma f' f'' - f f''') = f'''$$

$$2f''' + f f'' = 0$$

$$\text{i.e. } 2f_\alpha''' + f_\alpha f_\alpha'' = 0$$

ODE solved numerically subject BC.

$$BC: \quad u_1 = u_2 \quad v_x = 0 \quad \mu_1 u_{1y} = \mu_2 u_{2y} \quad y = 0$$

$$u_1 = \sigma_1 \quad u_2 = \sigma_2 \quad y = \pm \infty$$

$$ic \quad f_1'(0) = f_2'(0) \quad f_1(0) = f_2(0) = 0 \quad \mu_1 u_1 f_1'' \left[\frac{u_1}{\nu_1} \right]^{1/2}$$

$$= \mu_2 u_2 f_2'' \left[\frac{u_2}{\nu_2} \right]^{1/2}$$

$$f_1'(\infty) = \sigma_1 \quad f_2'(-\infty) = \frac{u_2}{\sigma_1} \quad ic \quad f_1'' [A \rho_1]^{1/2} = f_2'' [A \rho_2]^{1/2}$$

$$f_1''(0) = \left[\frac{\rho_2 \mu_1}{\rho_1 \mu_2} \right]^{1/2} f_2''(0)$$

$$= A^{1/2} f_2''(0)$$

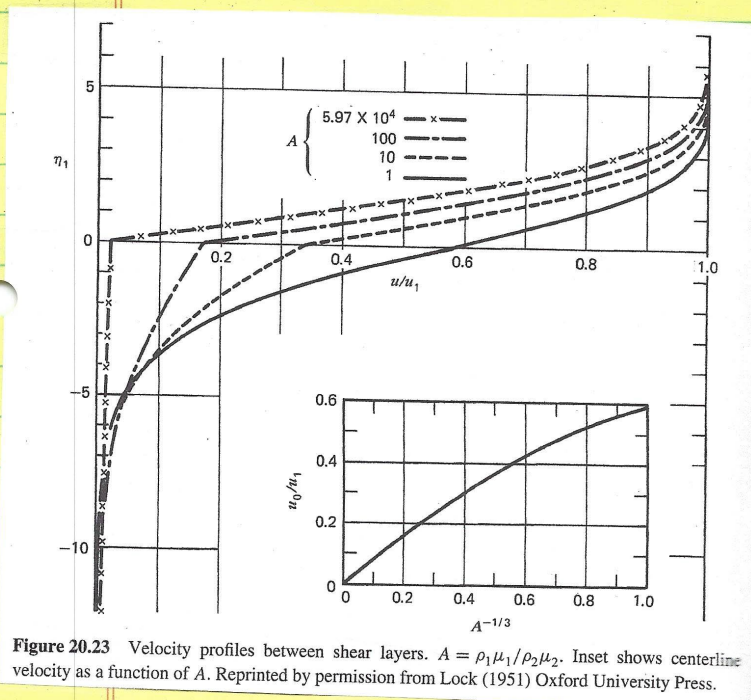


Figure 20.23 Velocity profiles between shear layers. $A = \rho_1 \mu_1 / \rho_2 \mu_2$. Inset shows centerline velocity as a function of A . Reprinted by permission from Lock (1951) Oxford University Press.

two uniform flows
arrive $x=0$ at
sudden merge.
 $P = \text{const}$ everywhere
 $u_1 > 0$ whereas
 $u_2 \geq 0$
 $y=0$ dividing x

$A = 5.97 \times 10^4 = \frac{\rho_2 \mu_1}{\rho_1 \mu_2}$
shown with $u_2 = 0$
Also other A values
down to 1 for which
 $u_1/u_2 = .58$ at $y=0$

Discontinuity smoothed by μ or more downstream to S shaped
free shear layer
Assume no mass transfer between fluids i.e. immiscible
Most practical cases: air/water or $\rho_2 \mu_2 = \rho_1 \mu_1$ i.e. same fluid
 $A \uparrow$ lower fluid moves more slowly - air-water also wind driven
motion (2) $f_2(-\infty)/\sqrt{2} = -.619$ = flat plate at $-\infty$ with BC from η_0
(2) $A = 1, v_2 = 0$: asymmetric, $u_1/u_2(0) > .5$ due differences convection upper/lower

Additional discussion

(2) For $\rho_1 \mu_1 \neq \rho_2 \mu_2$ jump fluid properties
 20°C datum at discontinuity at interface

	ρ	μ	ν	$\rho \mu$	$(\rho \mu)^{1/2}$
air	1.205	1.8×10^{-5}	1.5×10^{-5}		
water	1000	1.03×10^{-3}	1.005×10^{-6}		
	kg/m^3	Ns/m^2	m^2/s		
		kg/ms			
water/air	832	56	.067	46.592	216

∞ water/air jump condition mainly due ρ , which
 is reason sharp interface includes often
 very small ρ jump & smooth μ .

$$(2) \quad v_2 = \frac{1}{2} \left[\frac{v_2^2 u_1}{x} \right]^{1/2} [\gamma_2 f_2' - f_2] \quad \gamma_2 = [u_1 / v_2 x]^{1/2} y$$

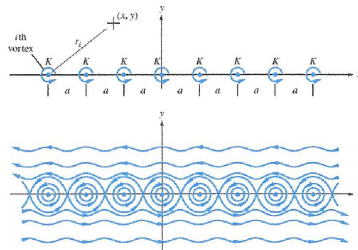
$$v_2(-\infty) = \frac{1}{2} \left[\frac{v_2^2 u_1}{x} \right]^{1/2} [(u_1 / v_2 x)^{1/2} (-\infty) \frac{v_2^2}{u_1} - f_2(\infty)]$$

(3) Interfacial complex diffusion under sheet
 $u_x = v u_y$ $u(x, 0) = U \operatorname{erf}(y)$ $u(x, t) = U$ $u(-\infty, t) = -U$
 $\delta = \pm 5.12 \sqrt{t}$ for $u = \pm .95U$ δ sheet profile but width $\pm U$

(4) Stability: linearized stability parallel viscous flow: $\Gamma_{\text{ext}} = 0$

Also related Kelvin-Helmholtz interfacial instability for
 horizontal interface dividing two ideal fluids with
 different ρ & μ is $\rho \nu$ & $\rho \mu$ jump at interface \Rightarrow vortex
 sheet

Potential flow solution for vortex sheet: Superposition infinite row equally spaced vortices of equal strength.



From afar (i.e. $y \geq a$) looks like a thin sheet with velocity discontinuity.

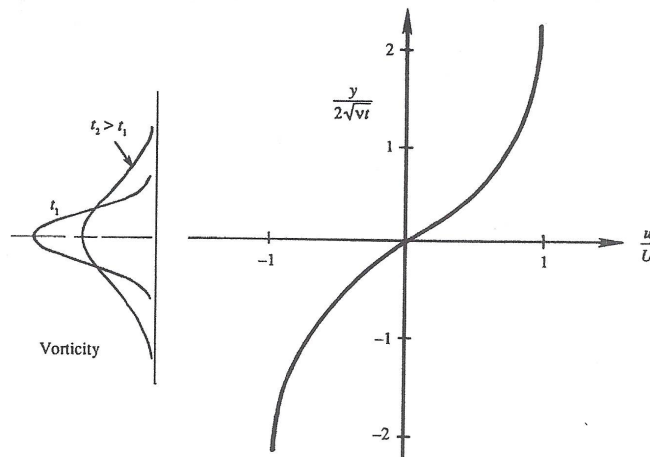
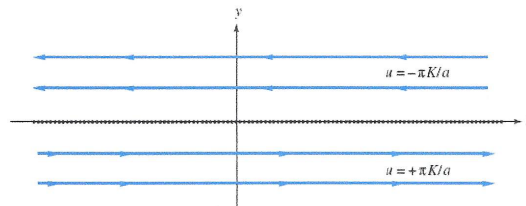


FIGURE 9.14 Viscous thickening of a vortex sheet. The left panel indicates the vorticity distribution at two times, while the right panel shows the velocity field solution in similarity coordinates. The upper half of this flow is equivalent to a temporally developing boundary layer.

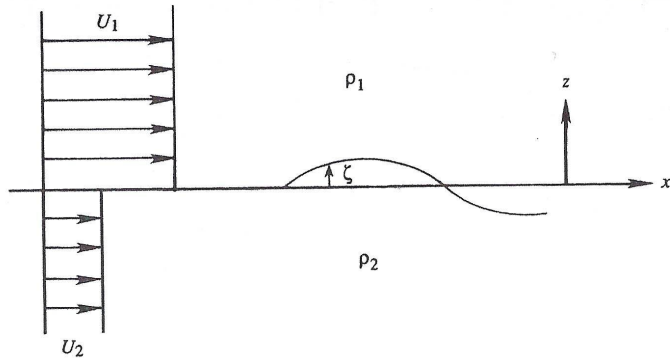


FIGURE 11.2 Basic flow configuration leading to the Kelvin-Helmholtz instability. Here the velocity and density profiles are discontinuous across an interface nominally located at $z = 0$. If the small vertical perturbation $\zeta(x,t)$ to this interface grows, then the flow is unstable.

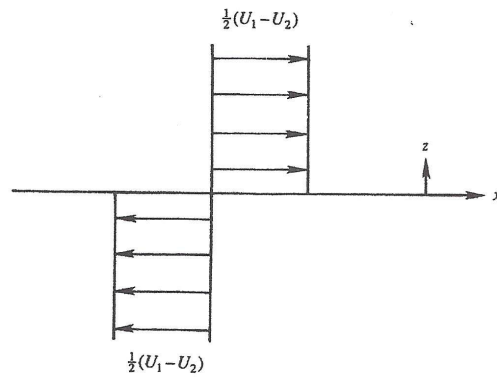


FIGURE 11.3 Background velocity field for the Kelvin-Helmholtz instability as seen by an observer traveling at the average velocity $(U_1 + U_2)/2$ of the two layers. When the densities of the two layers are equal, a disturbance to the interface will be stationary in this frame of reference.