

### Part 3: Momentum Integral Equation

Historically similarity and other AFD methods used for idealized flows and momentum integral methods for practical applications, including pressure gradients, but failure 3D methods motivated 3D BL theory which quickly progressed to modern day CFD.

Momentum integral equation, which is valid for both laminar and turbulent flow:

$$\int_{y=0}^{\infty} (\text{steady flow BL equation} + (u - U)\text{continuity}) dy$$

$$\frac{\tau_w}{\rho U^2} = \underbrace{\frac{1}{2} C_f}_{\text{For flat plate equation}} = \frac{d\theta}{dx} + (2 + H) \frac{\theta}{U} \frac{dU}{dx}$$

$$\theta = \int_0^{\delta} \frac{u}{U} \left(1 - \frac{u}{U}\right) dy$$

$$\delta^* = \int_0^{\delta} \left(1 - \frac{u}{U}\right) dy$$

$$H = \frac{\delta^*}{\theta}$$

$$\text{Momentum: } uu_x + vu_y = -\frac{\partial}{\partial x} \left(\frac{p}{\rho}\right) + \frac{1}{\rho} \frac{\partial \tau}{\partial y} \quad \text{where } \tau = \mu \frac{\partial u}{\partial y}$$

The pressure gradient evaluated from the outer potential flow using Bernoulli equation.

$$\begin{aligned} p + \frac{1}{2} \rho U^2 &= \text{constant} \\ p_x + \frac{1}{2} \rho 2UU_x &= 0 \\ -p_x/\rho &= UU_x \end{aligned}$$

$$(u - U) \underbrace{(u_x + v_y)}_{\text{Continuity}} = uu_x + uv_y - Uu_x - Uv_y$$

$$\underbrace{uu_x + vu_y - UU_x - \frac{1}{\rho} \tau_y}_{0} + \underbrace{uu_x + uv_y - Uu_x - Uv_y}_{0} = 0$$

$$\begin{aligned} -\frac{1}{\rho} \tau_y &= -2uu_x - vu_y + UU_x - uv_y + Uu_x + Uv_y \\ &= \frac{\partial}{\partial x} (uU - u^2) + (U - u)U_x + \frac{\partial}{\partial y} (vU - vu) \end{aligned}$$

$$\int_0^\infty -\frac{1}{\rho} \tau_y dy = -(\tau_w^0 - \tau_w)/\rho = \frac{\partial}{\partial x} \int_0^\infty u(U - u) dy + U_x \int_0^\infty (U - u) dy + (vU - vu)|_0^\infty$$

$$\begin{aligned} \frac{\tau_w}{\rho} &= \frac{\partial}{\partial x} \left[ U^2 \int_0^\infty \frac{u}{U} \left( 1 - \frac{u}{U} \right) dy \right] + U_x U \int_0^\infty \left( 1 - \frac{u}{U} \right) dy \\ &= U^2 \theta_x + 2UU_x \theta + UU_x \delta^* \end{aligned}$$

$$\frac{\tau_w}{\rho U^2} = \frac{1}{2} C_f = \theta_x + (2\theta + \delta^*) \frac{1}{U} \frac{dU}{dx}$$

$$\frac{C_f}{2} = \frac{d\theta}{dx} + (2 + H) \frac{\theta}{U} U_x$$

## METHODS Solution Momentum Integral Equation

Historically two approaches:

(1) One parameter velocity profiles

(2) Empirical correlations: Thwaites method

(1) Karman - Prandtl Method

①  $u(x, y) = U(x) f[y/\delta, \lambda(x)]$  guess form velocity profile

$$U_{\infty} = 2\gamma - 2\gamma^3 + \gamma^4 + \frac{\lambda}{6} [\gamma(1-\gamma)^2] \quad \gamma = y/\delta$$

② use  $\int_{BL}$  for  $U_{\infty}$

$$\lambda = \frac{\delta^2}{\sqrt{2}} U_{\infty}$$

③ compute:  $\theta, \delta^*, H, T_w$

= Prandtl

④ substitute momentum integral parameter  
equation for 1st order ODE  $\delta(x)$

⑤ with  $\delta(x)$  known all variables also known

Accuracy not as good Thwaites method

Issues:

Recall very quadratic guess profile  
flat plate velocity profile off 10% accuracy.

Accuracy depends type of guess profile.

TABLE 4.1

Boundary-layer predictions from five piecewise analytic profiles with their errors relative to the classic Blasius values

	$\frac{U}{U} = F(\xi)$	$\eta^0 = \frac{\delta^0}{\delta}$	$\theta^0 = \frac{\theta}{\delta}$	$H = \frac{\delta^0}{\theta}$	$\frac{\delta}{x} \sqrt{Re_x}$	$C_f \sqrt{Re_x} = \frac{\delta^0}{x} \sqrt{Re_x}$	$L_2$ error
1	$2\xi - \xi^2$	0.333 3.1%	0.133 0.25%	2.500 3.5%	5.477 9.5%	0.730 10%	1.826 6.1%
2	$\frac{1}{3}\xi^2 - \frac{1}{2}\xi^3$	0.375 9.0%	0.139 4.7%	2.692 4.0%	4.641 7.2%	0.646 2.6%	1.740 1.1%
3	$2\xi - 2\xi^2 + \xi^4$	0.300 13%	0.118 12%	2.554 1.4%	5.836 17%	0.685 3.2%	1.751 1.8%
4	$\sin\left(\frac{1}{2}\xi^2\right)$	0.363 5.6%	0.137 2.7%	2.660 2.7%	4.795 4.1%	0.655 1.3%	1.743 1.3%
5	$\frac{1}{3}\xi^2 - \xi^3 + \frac{1}{3}\xi^4$	0.350 1.7%	0.134 0.52%	2.618 1.1%	4.993 0.13%	0.668 0.53%	1.748 1.6%
	Blasius (1908)	0.344	0.133	2.59	5	0.664	1.72
						n/a	

$$L_2 = \left[ \int_0^1 (F - F_{\text{Blasius}})^2 dy \right]^{1/2}$$

1, 2, 3 Pohlhausen (1921)

4 Schlichting (1979)

5 Migeleau et Xuem (2020)

Pohlhausen paradox: increasing order, i.e., # BC profile can satisfy does not improve accuracy

BC:  $u(x, 0) = 0$  1 no slip

$u(x, \delta) = U$  2 match

$u_y(x, \delta) = 0$  3 smooth merge  $U$

$\mu u_{yy}(x, 0) = p_x$  4 correct balance momentum  $y=0$

$\tau_{xy}(y, \delta) = 0$  5 zero shear stress at  $\delta$

However, the Blasius profile does not in fact satisfy all these conditions!

Note 1 satisfying 1-3 & 2-5 satisfying 1-4  
 but only 3 satisfies 1-5  
 enlarges BC error

$B\zeta \leq 5$  true at  $y \rightarrow \infty$  but not true  $y=5$   
 where  $\frac{dy}{dx} = -0.7085$

Blasius

Also higher initial  
 Slope  $F'(0)$

Other differences  
 such as  $F(1) \neq F'(1)$

TABLE 4.2

Endpoint properties of the piecewise analytic velocity profiles and their corresponding Blasius values

$\frac{U}{U} = F(\xi)$	$F(0)$	$F'(0)$	$F''(0)$	$F(1)$	$F'(1)$	$F''(1)$
$2\xi - \xi^2$	0	2.000	-2	1.000	0	-2.000
$\frac{3}{2}\xi - \frac{1}{2}\xi^3$	0	1.500	0	1.000	0	-3.000
$2\xi - 2\xi^2 + \xi^4$	0	2.000	0	1.000	0	0.000
$\sin\left(\frac{1}{2}\pi\xi\right)$	0	1.571	0	1.000	0	-2.467
$\frac{5}{3}\xi - \xi^3 + \frac{1}{3}\xi^5$	0	1.667	0	1.000	0	-2.000
Blasius (1908)	0	1.630	0	0.990	0.0904	-0.709

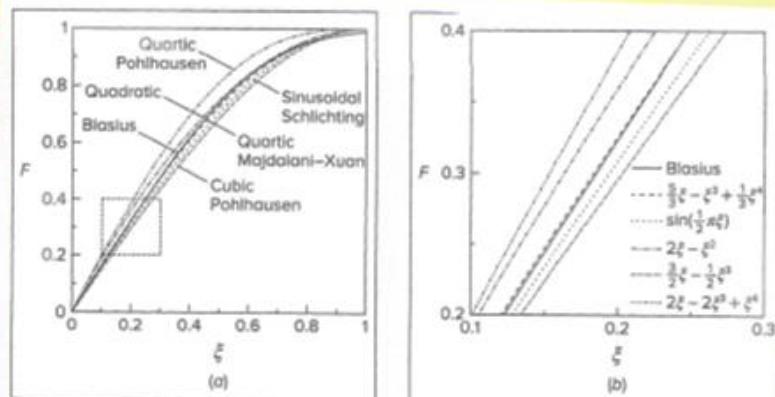


FIGURE 4-5  
 Comparison of five analytic approximations to the Blasius solution (solid line) including Pohlhausen's quadratic, cubic, and quartic polynomials (chained lines) as well as Schlichting's sinusoidal (dotted) and Majdalani-Xuan's quartic (dashed) profiles across (a) the boundary layer and (b) a designated quadrant where individual deviations from the Blasius curve are magnified.

Presumably these differences compounded  
 for  $P_x \neq 0$ .

## Thwaites Method (1949)

Pressure gradient parameter  $\lambda = \frac{\theta^2}{\nu} \frac{dU}{dx} = (\frac{\theta}{\delta})^2 \Lambda$  where  $\Lambda = \frac{\delta^2}{\nu} \frac{dU}{dx} = -p_x \frac{\delta^2}{\mu U}$  is the Pohlhausen parameter.

Multiply momentum integral equation by  $\frac{U\theta}{\nu}$

$$\frac{\tau_w \theta}{\mu U} = \frac{U\theta}{\nu} \frac{d\theta}{dx} + \frac{\theta^2}{\nu} \frac{dU}{dx} (2 + H)$$

The equation is dimensionless and, LHS and H can be correlated with  $\lambda$  as shear and shape-factor correlations:

$$\frac{\tau_w \theta}{\mu U} = S(\lambda) = (\lambda + 0.09)^{0.62}$$

$$H = \delta^*/\theta = H(\lambda) = \sum_{i=0}^5 a_i (0.25 - \lambda)^i$$

$$a_i = (2, 4.14, -83.5, 854, -3337, 4576)$$

Note

$$\frac{U\theta}{\nu} \frac{d\theta}{dx} = \frac{1}{2} U \frac{d}{dx} \left( \frac{\theta^2}{\nu} \right)$$

Substitute above into momentum integral equation.

$$S(\lambda) = \frac{1}{2} U \frac{d}{dx} \left( \frac{\theta^2}{\nu} \right) + \lambda(2 + H)$$

$$U \frac{d(\lambda/U_x)}{dx} = 2[S - \lambda(2 + H)\lambda] = F(\lambda)$$

$$F(\lambda) = 0.45 - 6\lambda \text{ based on AFD and EFD}$$

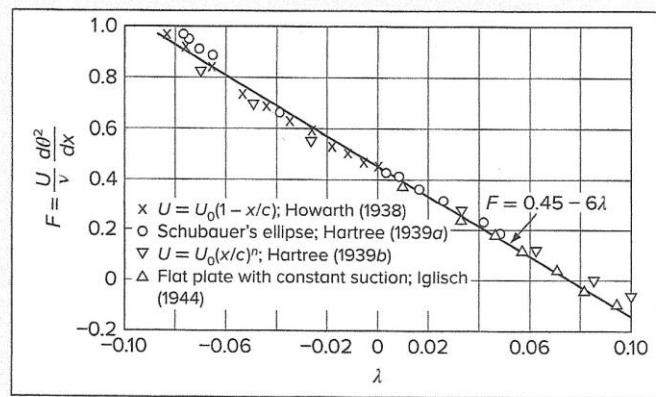


FIGURE 4-27  
Empirical correlation of the boundary-layer function in Eq. (4-156). [After Thwaites (1949).]

Define  $z = \frac{\theta^2}{\nu}$  so that  $\lambda = z \frac{dU}{dx}$

$$U \frac{dz}{dx} = 0.45 - 6\lambda = 0.45 - 6z \frac{dU}{dx}$$

$$U \frac{dz}{dx} + 6z \frac{dU}{dx} = 0.45$$

$$\frac{1}{U^5} \frac{d}{dx} (zU^6) = U \frac{dz}{dx} + 6z \frac{dU}{dx} = 0.45$$

$$d(zU^6) = 0.45U^5 dx$$

$$zU^6 = 0.45 \int_0^x U^5 dx + C$$

$$\rightarrow \theta^2 = \theta_0^2 + \frac{0.45\nu}{U^6} \int_0^x U^5 dx$$

$\theta_0(x = 0) = 0$  and  $U(x)$  known from potential flow solution.

Complete solution:

$$\lambda = \lambda(\theta) = \frac{\theta^2}{\nu} \frac{dU}{dx}$$

$$\frac{\tau_w \theta}{\mu U} = S(\lambda)$$

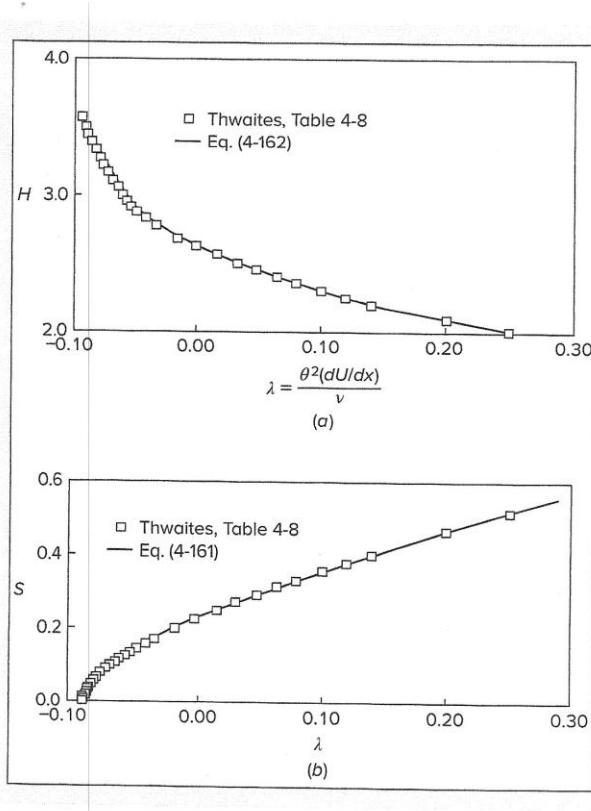
$$\delta^* = \theta H(\lambda)$$

Accuracy: mild  $p_x \pm 5\%$  and strong adverse  $p_x$  ( $\tau_w$  near 0)  $\pm 15\%$

**TABLE 4-8**

**Shear and shape functions correlated by Thwaites (1949)**

$\lambda$	$H(\lambda)$	$S(\lambda)$	$\lambda$	$H(\lambda)$	$S(\lambda)$
+0.25	2.00	0.500	-0.056	2.94	0.122
0.20	2.07	0.463	-0.060	2.99	0.113
0.14	2.18	0.404	-0.064	3.04	0.104
0.12	2.23	0.382	-0.068	3.09	0.095
0.10	2.28	0.359	-0.072	3.15	0.085
+0.080	2.34	0.333	-0.076	3.22	0.072
0.064	2.39	0.313	-0.080	3.30	0.056
0.048	2.44	0.291	-0.084	3.39	0.038
0.032	2.49	0.268	-0.086	3.44	0.027
0.016	2.55	0.244	-0.088	3.49	0.015
0.0	2.61	0.220	-0.090	3.55	0.000
(Separation)					
-0.016	2.67	0.195			
-0.032	2.75	0.168			
-0.040	2.81	0.153			
-0.048	2.87	0.138			
-0.052	2.90	0.130			



**FIGURE 4-28**  
The laminar boundary-layer correlated functions by Thwaites (1949): (a) shape factor; (b) shear stress with curve fits.

Separation predicted within 4%; however, large scale separation causes viscous/inviscid interaction and alters imposed external  $U(x)$  and  $p_x(x)$

**TABLE 4-9**  
Laminar-separation-point prediction by Thwaites' method

$U(x)$	$x_{\text{sep}}$ (exact)	Thwaites	
		$x_{\text{sep}}$	Error [%]
Howarth (1938)			
$1 - x$	0.120	0.123	+2.5
Tani (1949)			
$1 - x^2$	0.271	0.268	-1.1
$1 - x^4$	0.462	0.449	-2.8
$1 - x^8$	0.640	0.621	-3.0
Terrill (1960)			
$\sin(x)$	1.823	1.800	-1.3
Curle (1958)			
$x - x^3$	0.655	0.648	-1.1
Görtler (1957)			
$\cos(x)$	0.389	0.384	-1.3
$(1 - x)^{1/2}$	0.218	0.221	+1.3
$(1 - x)^2$	0.0637	0.0652	+2.4
$(1 + x)^{-1}$	0.151	0.158	+4.6
$(1 + x)^{-2}$	0.0713	0.0739	+3.6

## Pohlhausen Velocity Profile:

$$\frac{u}{U} = f(\eta) = a\eta + b\eta^2 + c\eta^3 + d\eta^4 \text{ with } \eta = \frac{y}{\delta}$$

a, b, c, d determined from boundary conditions:

$$1) y = 0 \rightarrow u = 0, u_{yy} = -\frac{U}{\nu} U_x$$

$$2) y = \delta \rightarrow u = U, u_y = 0, u_{yy} = 0$$

$$\Rightarrow \frac{u}{U} = F(\eta) + \Lambda G(\eta), -12 \leq \Lambda \leq 12 \quad \Lambda = \frac{\delta^2}{\nu} \frac{dU}{dx} = -p_x \frac{\delta^2}{\mu U}$$

↑  
separation      (experiment:  $\Lambda_{separation} = -5$ )

$$F(\eta) = 2\eta - 2\eta^3 + \eta^4$$

$$G(\eta) = \frac{\eta}{6}(1-\eta)^3$$

$$\lambda = \lambda(\Lambda) = \left( \frac{37}{315} - \frac{\Lambda}{945} + \frac{\Lambda^2}{9072} \right) \Lambda$$

Profiles are realistic, except near separation. In guessed profile methods  $u/U$  directly used to solve momentum integral equation numerically, but accuracy not as good as empirical correlation methods; therefore, use Thwaites method to get  $\lambda$ , etc., and then use  $\lambda$  to get  $\Lambda$  and plot  $u/U$ .

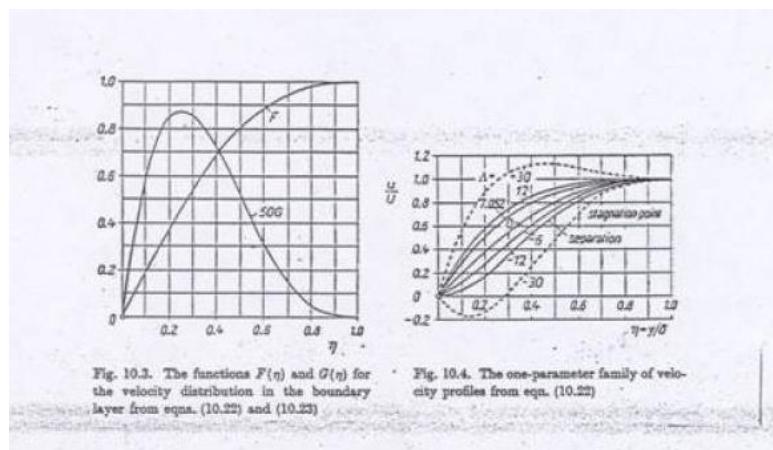
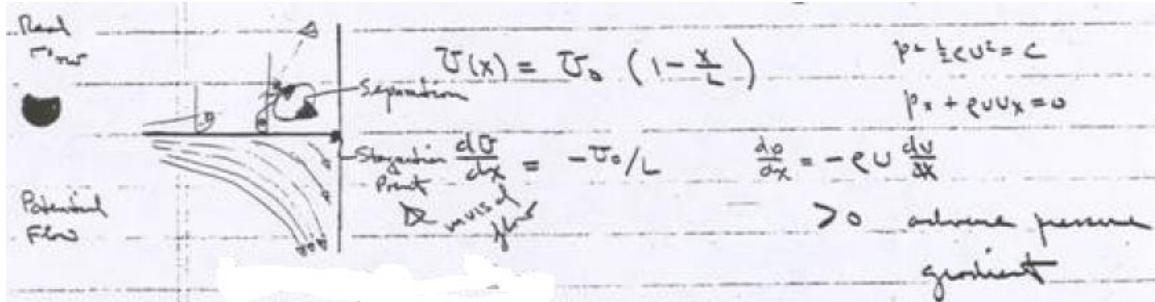


Fig. 10.3. The functions  $F(\eta)$  and  $G(\eta)$  for the velocity distribution in the boundary layer from eqns. (10.22) and (10.23)

Fig. 10.4. The one-parameter family of velocity profiles from eqn. (10.22)

## Howarth linearly decelerating flow (example of exact solution of steady state 2D boundary layer)



Howarth proposed a linearly decelerating external velocity distribution  $U(x) = U_0 \left(1 - \frac{x}{L}\right)$  as a theoretical model for laminar boundary layer study. Use Thwaites's method to compute:

- a)  $X_{sep}$
- b)  $C_f \left(\frac{x}{L} = 0.1\right)$

Note  $U_x = -U_0/L$

Solution

$$\theta^2 = \frac{0.45\nu}{U_0^6 \left(1 - \frac{x}{L}\right)^6} \int_0^x U_0^5 \left(1 - \frac{x}{L}\right)^5 dx = 0.075 \frac{\nu L}{U_0} \left[ \left(1 - \frac{x}{L}\right)^{-6} - 1 \right]$$

can be evaluated for given  $L, Re_L$

$$\lambda = \frac{\theta^2}{\nu} \frac{dU}{dx} = -0.075 \left[ \left(1 - \frac{x}{L}\right)^{-6} - 1 \right]$$

$$\lambda_{sep} = -0.09 \Rightarrow \frac{X_{sep}}{L} = 0.123$$

3% higher than exact solution = 0.1199

$C_f \left( \frac{x}{L} = 0.1 \right) \Rightarrow$  i.e. just before separation

$$\lambda = -0.0661$$

$$S(\lambda) = 0.099 = \frac{1}{2} C_f Re_\theta$$

$$C_f = \frac{2(0.099)}{Re_\theta}$$

Compute  $Re_\theta$  in terms of  $Re_L$

$$\theta^2 = 0.075 \frac{\nu L}{U_0} \left[ (1 - 0.1)^{-6} - 1 \right] = 0.0661 \frac{\theta L}{U_0}$$

$$\frac{\theta^2}{L^2} = 0.0661 \frac{\nu L}{U_0} = \frac{0.0661}{Re_L}$$

$$\frac{\theta}{L} = \frac{0.257}{Re_L^{1/2}}$$

$$Re_\theta = \frac{\theta}{L} Re_L = 0.257 Re_L^{1/2}$$

$$C_f = \frac{2(0.099)}{0.257} Re_L^{-1/2} = 0.77 Re_L^{-1/2}$$

To complete  
solution must  
specify  $Re_L$

Consider the complex potential

$$F(z) = \frac{a}{2} z^2 = \frac{a}{2} r^2 e^{2i\theta}$$

$$\varphi = \operatorname{Re}[F(z)] = \frac{a}{2} r^2 \cos 2\theta$$

$$\psi = \operatorname{Im}[F(z)] = \frac{a}{2} r^2 \sin 2\theta$$

Orthogonal rectangular hyperbolas

$\varphi$ : asymptotes  $y = \pm x$

$\psi$ : asymptotes  $x=0, y=0$

$$\left\{ \begin{array}{l} V = \nabla \varphi = \varphi_r \hat{e}_r + \frac{1}{r} \varphi_\theta \hat{e}_\theta \\ v_r = ar \cos 2\theta \\ v_\theta = -ar \sin 2\theta \end{array} \right. \quad \frac{\pi}{2} \leq \theta \leq 0 \text{ (flow direction as shown)}$$

$$V = v_r (\cos \theta \hat{i} + \sin \theta \hat{j}) + v_\theta (-\sin \theta \hat{i} + \cos \theta \hat{j}) = (v_r \cos \theta - v_\theta \sin \theta) \hat{i} + (v_r \sin \theta + v_\theta \cos \theta) \hat{j}$$

Potential flow slips along surface: (consider  $\theta = 90^\circ$ )

1) determine  $a$  such that  $v_r = U_0$  at  $r=L$ ,  $\theta = 90^\circ$

$$v_r = aL \cos(2 \times 90) = U_0 \Rightarrow aL = -U_0, \text{ i.e. } a = -\frac{U_0}{L}$$

2) let  $U(x) = v_r$  at  $x=L-r$ :

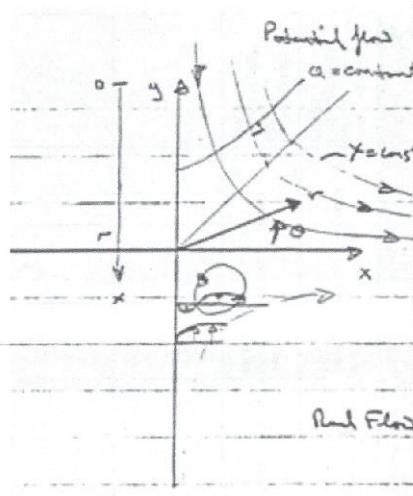
$$\Rightarrow v_r = a(L-x) \cos(2 \times 90) = U(x)$$

$$\text{Or: } U(x) = -a(L-x) = \frac{U_0}{L}(L-x) = U_0 \left(1 - \frac{x}{L}\right) \quad U_x = -\frac{U_0}{L}$$

$$\rho + \frac{1}{2} \rho U^2 = C$$

$$\rho_x + \rho U U_x = 0$$

$$\rho_x = -\rho U U_x = -\rho U_0 \left(1 - \frac{x}{L}\right) \left(-\frac{U_0}{L}\right) = \rho \frac{U_0^2}{L} \left(1 - \frac{x}{L}\right)$$



$$\begin{aligned} \gamma &= \beta xy & \beta &= U/L \\ u &= \beta x = \gamma_y & u &= \beta y = -\gamma_x \\ v &= -\beta y = -\gamma_x & p + \frac{1}{2} \rho (u^2 + v^2) &= C \\ p + \frac{1}{2} \rho \beta^2 (x^2 + y^2) &= C & p(x_0, 0) &= C = p_0 \\ p &= p_0 - \frac{1}{2} \rho \frac{U_0^2}{L^2} (x^2 + y^2) & p_x &= -\rho \frac{U_0^2}{L^2} x \\ p_x &= -\rho \frac{U_0^2}{L^2} y & p_y &= -\rho \frac{U_0^2}{L^2} x \end{aligned}$$

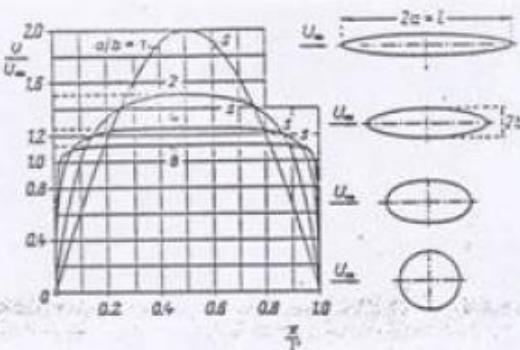


Fig. 10.9. Potential velocity distribution function on elliptical cylinders of slenderness  $a/b = 1, 2, 4, 8$ , the direction of the stream being parallel to the major axis  
 $\xi =$  position of point of separation

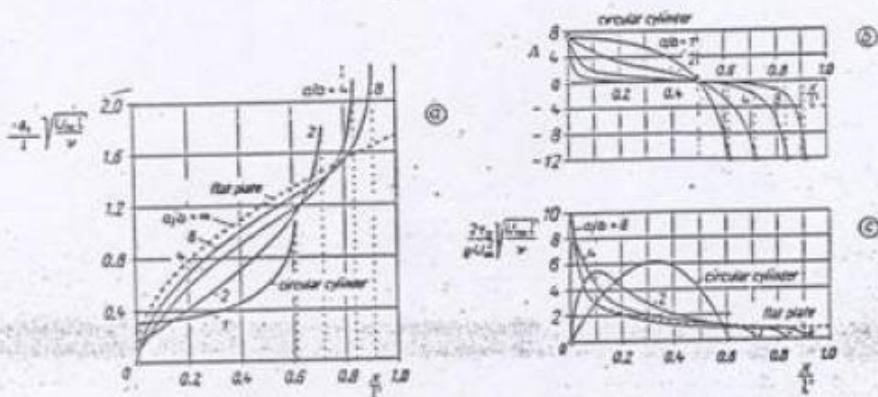


Fig. 10.10. Results of the calculation of boundary layers on elliptical cylinders of slenderness  $a/b = 1, 2, 4, 8$ . Fig. 10.9. a) displacement thickness of the boundary layer, b) shape factor  $\psi(l/d)$ , c) shearing stress at the wall,  $2 \tau_w$  — circumference of the ellipse;  $a/b = 1$  circular cylinder;  $a/b = \infty$  flat plate

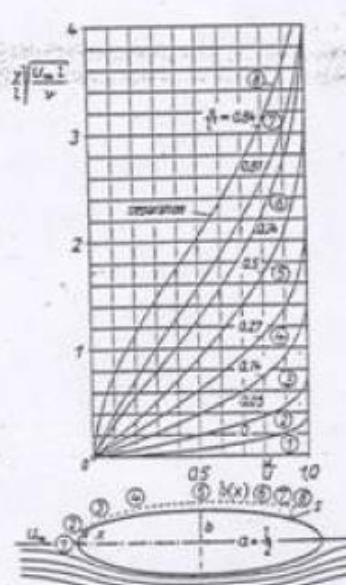


Fig. 10.11. Velocity profiles in the laminar boundary layer on an elliptical cylinder. Ratio of axes  $a/b = 4$

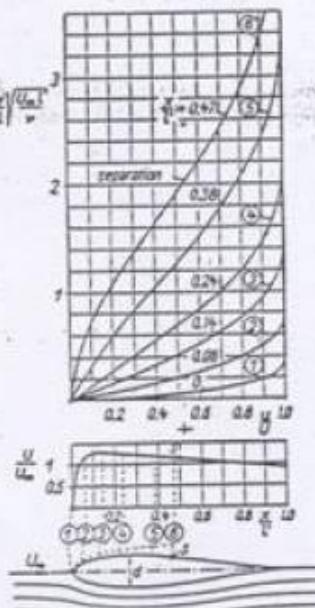


Fig. 10.12. Velocity profiles in the laminar boundary layer and potential velocity function for a Zhukovskii aerofoil J 015 of thickness ratio  $d/l = 0.15$  at an angle of incidence  $\alpha = 0$

Refer back  
to Table 4-6  
(Sec 26) with  
regards relative  
performance of  
wing sections

## Minimum deviation momentum integral equation $\#1$

$$u_x + u_y = 0$$

$$(u^2)_x + (uu)_y = uu_x + \sqrt{u} \frac{\partial u}{\partial y} \quad 2uu_x + u_y u + \underbrace{u_{yy}}_{-u_x u} = R.H.S.$$

$$u(x, 0) = 0$$

$$u(x, S) = U(x)$$

$$-uu_x + uu_y = R.H.S$$

$$\mu u_y(x, 0) = T_0 = T_W \quad u_y(x, S) = 0 \quad T = \mu u_y \Rightarrow \sqrt{u} u_y = \frac{T}{\rho}$$

$$\int_0^S [(u^2)_x + (uu)_y] dy = \int_0^S [uu_x + \sqrt{u} u_y] dy$$

$$\int_0^S (u^2)_x dy + \cancel{uu(u, S)} = uu_x \int_0^S dy - T_0/\rho \quad U \neq f(y) \text{ but} \\ \int_0^S -u_x dy \quad \text{reduced integral} \\ \text{to obtain desired}$$

$$\int_0^S (u^2)_x dy - U \int_0^S u_x dy = uu_x \int_0^S dy - T_0/\rho \quad \text{form integral} \\ \int_{x_0}^S \cancel{u_x dy} \quad \text{equation}$$

$$\text{Leibniz rule: } \int_0^S u_x dy = \frac{du}{dx} \int_0^S u dy + u(x, 0) \frac{du}{dx} - u(S, S) \frac{du}{dx}$$

$$\int_0^S (u^2)_x dy = \frac{du}{dx} \int_0^S u^2 dy - U^2 S_x$$

$$\int_0^S u_x dy = \frac{du}{dx} \int_0^S u dy - U S_x$$

$$\frac{du}{dx} \int_0^S u^2 dy - U^2 S_x - U \frac{du}{dx} \int_0^S u dy + U^2 S_x = uu_x \int_0^S dy - T_0/\rho \\ = \frac{du}{dx} \int_0^S uu_x dy - uu_x \int_0^S u dy$$

$$\frac{du}{dx} \int_0^S u^2 dy - \frac{du}{dx} \int_0^S uu_x dy + uu_x \int_0^S u dy = uu_x \int_0^S dy - T_0/\rho$$

$$\frac{1}{\delta} \int_0^\delta u(\tau-u) dy + \bar{U}_x \int_0^\delta (\tau-u) dy = I_0/\rho$$

$$\frac{1}{\delta} \left[ U^2 \int_0^\infty \underbrace{\frac{y}{\delta} (1 - \frac{y}{\delta}) dy}_{\textcircled{1}} \right] + \bar{U}_x U \int_0^\infty \underbrace{(1 - \frac{y}{\delta}) dy}_{\textcircled{2}} = I_0/\rho$$

since from  $\delta \rightarrow \infty$   $U-u=0$

$$\frac{1}{\delta} (U^2 \textcircled{1}) + \bar{U}_x U \textcircled{2} = I_0/\rho$$

$$\text{or } 2U\bar{U}_x \delta + U^2 \textcircled{1} + \bar{U}_x U \textcircled{2} = I_0/\rho$$

$$\textcircled{1} + (2\delta + \delta^2) \bar{U}_x / U = I_0/\rho U^2 = \zeta_f/2$$

$$\textcircled{2} + (2 + H) \frac{\textcircled{1}}{U} \bar{U}_x = \zeta_f/2 \quad H = \delta^2/\rho$$

Assume  $u(x,y) \Rightarrow \alpha, \delta^*, I_0 \Rightarrow f(\delta)$  then  
solve momentum integral for  $\delta(x)$ .

<sup>+ M order</sup>  
Karmen-Pohl momentum profile  
is classical approach, which also  
uses empirical corrections.

### Karman-Pohlhausen Method

$$u/v = a + b\gamma + c\gamma^2 + d\gamma^3 + e\gamma^4 \quad \gamma(x, y) = y/\delta(x)$$

where  $a - c = f(x)$  is self similar not possible

$$u(x, 0) = 0 \quad u(x, \delta) = f(x)$$

$$u_y(x, 0) = 0 \quad u_{yy}(x, 0) = -\frac{f''(x)}{\delta} \quad u_{yy}(y, \delta) = 0$$

3L momentum |  $y=0$

or in terms of  $u/v = f(\gamma)$

$$\frac{\partial}{\partial y} \left( \frac{u}{v} \right)_y = -\frac{\delta^2}{v} \delta_x = -f''(x) \quad \gamma = 0$$

$$\frac{\partial}{\partial y} \left( \frac{u}{v} \right)_y = \left( \frac{u}{v} \right)_{yy} = 0 \quad \gamma = 1$$

$$\frac{\partial}{\partial y} \left( \frac{u}{v} \right)_y = \frac{\partial}{\partial y} \left( \frac{\partial}{\partial y} \left( \frac{u}{v} \right)_y \right)^2 = \frac{\partial^2}{\partial y^2} \left( \frac{u}{v} \right)_y = \frac{\partial^2}{\partial y^2} \delta^{-2}$$

$$u_{yy} = \frac{\partial}{\partial y} \delta^{-2} (u/v) = u_{yy} \delta^{-2} v$$

$$\delta^2 u_{yy}/v = u_{yy} = -\frac{\delta^2 \delta_x}{v} \frac{\delta^{-2}}{\delta} = -\frac{\delta^2}{v} \delta_x = -f''(x)$$

$$0 = a \quad 1$$

$$-f'' = 2c \quad 2 \quad \left( \frac{u}{v} \right)_{yy} = b + 2c\gamma + 3\lambda\gamma^2 + 4\gamma^3 \quad \text{measure } \delta_x \text{ under flow}$$

$$2 = a + 2c + \lambda + c \quad 3 \quad \left( \frac{u}{v} \right)_{yy} = 2c + 6\lambda\gamma + 12\gamma^2 \Big|_{\gamma=0} = c$$

$$0 = b + 2c + 3\lambda + 4c \quad 4$$

$$0 = 2c + 6\lambda + 12c \quad 5$$

$$a = 0 \quad b = \frac{1}{2} + \frac{\lambda}{6} \quad c = -\frac{\lambda}{2} \quad \lambda = -2 + \frac{\lambda}{2} \quad c = 1 - \frac{\lambda}{6}$$

$$0 = -f'' + 6\lambda + 12c \quad 0 = \lambda - f'' + \lambda/2 - 6c + 4c \quad 2 = \frac{\lambda}{2} + 2\lambda - \frac{\lambda}{2} + \frac{\lambda}{6} - 3c + c$$

$$\lambda = (\lambda - 12c)/6 = \lambda/2 + 2c \quad c = 1 - \lambda/6$$

$$\lambda/6 - 2c \quad \lambda/2 + 2 - \frac{\lambda}{3} = 2 + \frac{\lambda}{6}$$

$$= \lambda/6 - 2 + \frac{\lambda}{6} = -2 + \lambda/2$$

$$\begin{aligned} u/\sigma &= (2 + \frac{\Delta}{2})\eta - \frac{1}{2}\eta^2 + (-2 + \frac{\Delta}{2})\eta^3 + (1 - \frac{\Delta}{2})\eta^4 \\ &= (2\eta - 2\eta^3 + \eta^4) + \frac{\Delta}{2}(\eta - 3\eta^2 + 3\eta^3 - \eta^4) \\ &= 2 - (1+\eta)(1-\eta)^3 + \frac{\Delta}{6}\eta(1-\eta)^3 \\ u/\sigma &= F(\eta) + \Delta G(\eta) \end{aligned}$$

$$\begin{aligned} (1-\eta)(1-\eta)^3 &= ((1-2\eta + \eta^2)(1-\eta)) = 1 - 2\eta + \eta^2 - \eta + 2\eta^2 - \eta^3 \\ &= 1 - 3\eta + 3\eta^2 - \eta^3 \\ (1-3\eta + 3\eta^2 - \eta^3)(1-\eta) &= 1 - 3\eta + 3\eta^2 - \eta^3 + \eta - 3\eta^2 + 3\eta^3 - \eta^4 \\ &= 1 - 2\eta + 2\eta^3 - \eta^4 \\ 1 - \Delta G(\eta) &= 2\eta - 2\eta^3 + \eta^4 \end{aligned}$$

$F(\eta)$  monotonically increasing  
 $F(\eta) \quad 0 \leq F \leq 1$

$$G(\eta) \text{ of } \eta \text{ more} = .0166 |$$

$\eta=0$	$\eta=.25$
$\rightarrow 0$	$\rightarrow 1$

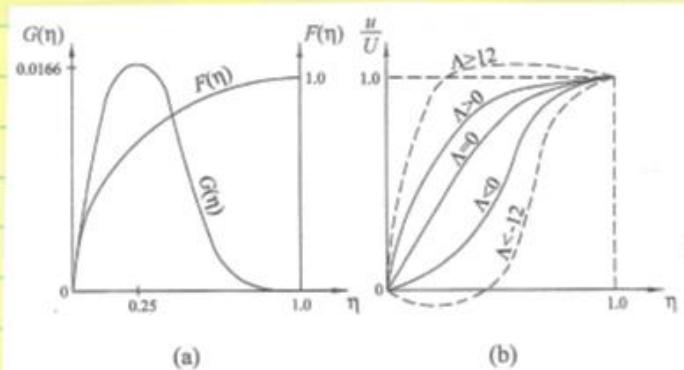


FIGURE 9.6 (a) Form of the functions  $F(\eta)$  and  $G(\eta)$ , and (b) the velocity profiles for various values of the parameter  $\Delta(x)$ .

$\Delta \quad u/\sigma$

$\Delta = 0$  4th order

polynomial approximation

blowup

$\Delta > 12$  overshoot not physical so it is restricted  $\Delta < 12$

$\Delta < -12$  reverse flow in separation, which violates

BL theory

Conclusion:  $-12 < \Delta(x) < 12$

$$\begin{aligned}\delta^* &= \int_0^\delta (1 - \frac{\eta}{\delta}) d\gamma & \gamma = \eta/\delta \quad d\gamma = d\eta/\delta \\ &= \delta \int_0^1 (1 - \frac{\eta}{\delta}) d\eta & \eta=0 \quad \gamma=0 \quad \eta=\delta \quad \gamma=1 \\ &= \delta \int_0^1 [(\eta)(1-\eta)^2 - \frac{1}{6} \eta (1-\eta)^3] d\eta = \delta \left( \frac{3}{10} - \frac{1}{120} \right) \\ \Theta &= \delta \int_0^1 \frac{\partial}{\partial \eta} (1 - \frac{\eta}{\delta}) d\eta = \delta \left( \frac{3\gamma}{315} - \frac{1}{945} - \frac{\lambda^2}{9075} \right)\end{aligned}$$

$$\begin{aligned}I_0 &= \mu \frac{\partial \eta}{\partial \gamma} \Big|_{\gamma=0} = \mu \frac{\partial \eta}{\partial \gamma} \Big|_{\gamma=0} = \mu \frac{\eta}{\delta} \frac{\partial \eta / \delta}{\partial \gamma} \Big|_{\gamma=0} \\ &= \mu \frac{\eta}{\delta} \frac{\partial}{\partial \gamma} \left[ 1 - (\eta)(1-\eta)^2 + \frac{1}{6} \eta (1-\eta)^3 \right] \Big|_{\gamma=0} \\ &= \mu \frac{\eta}{\delta} \left( 2 + \frac{\lambda^2}{6} \right)\end{aligned}$$

$\delta^*, \Theta, I_0 = f(\delta)$   $\delta$  determines momentum integral equation

$$\frac{v_0}{\nu} \Theta_x + (2\omega + \delta^*) \frac{\Theta}{\nu} U_x = \frac{I_0}{\mu} \frac{\Theta}{\nu} \quad \frac{\partial \Theta}{\partial x} \xrightarrow{\downarrow}$$

$$\frac{1}{2} U \frac{\partial}{\partial x} \left( \frac{\Theta^2}{\nu} \right) + (2 + \frac{\delta^*}{\delta}) \frac{\Theta^2}{\nu} U_x = \frac{I_0 \Theta}{\mu \nu}$$

$$L = \frac{I_0}{\nu} U_x \quad i.e. \quad \frac{\Theta^2}{\nu} U_x = \frac{\Theta^2}{\delta^2} L = \left( \frac{3\gamma}{315} - \frac{1}{945} - \frac{\lambda^2}{9075} \right) L = k(x)$$

$$\text{Also } \frac{\delta^*}{\delta} = \frac{\left( \frac{3}{10} - \frac{1}{120} \right)}{\left( \frac{3\gamma}{315} - \frac{1}{945} - \frac{\lambda^2}{9075} \right)} = f(k) \quad \tilde{f} = f(L(x))$$

also  $k(x) \neq 0$

consider  $f = f(k)$

$$\frac{I_0 \Theta}{\mu \nu} = \underbrace{(2 + \frac{\lambda^2}{\delta})}_{\frac{I_0 \Theta}{\mu \nu}} \underbrace{\left( \frac{3\gamma}{315} - \frac{1}{945} - \frac{\lambda^2}{9075} \right)}_{\Theta/L} = g(k)$$

functionality of  
some reasoning  $f$

$$\frac{1}{2} \nabla \cdot \frac{1}{\lambda} \nabla \left( \frac{\Theta^2}{\lambda} \right) + [z + f(\lambda)] \lambda = g(\lambda) \quad \lambda = \frac{\Theta^2}{\lambda} \nabla \cdot \lambda$$

let  $\tilde{z} = \frac{\Theta^2}{\lambda}$  = new dependent variable i.e.  $\lambda = z \nabla \cdot \lambda$

$$\nabla \cdot \lambda = \frac{\Theta^2}{\lambda} = H(\lambda) \quad \lambda = z \nabla \cdot \lambda = H(\lambda)$$

$$H(\lambda) = 2 \left\{ \left( 2 + \frac{\Lambda}{6} \right) \left( \frac{37}{315} - \frac{\Lambda}{945} - \frac{\Lambda^2}{9,072} \right) \right. \\ \left. - \left[ 2 + \frac{\left( \frac{1}{10} - \frac{\Lambda}{120} \right)}{\left( \frac{37}{315} - \frac{\Lambda}{945} - \frac{\Lambda^2}{9,072} \right)} \right] \left( \frac{37}{315} - \frac{\Lambda}{945} - \frac{\Lambda^2}{9,072} \right)^2 \Lambda \right\} \\ = 2 \left( \frac{37}{315} - \frac{\Lambda}{945} - \frac{\Lambda^2}{9,072} \right) \left[ 2 - \frac{116}{315} \Lambda + \left( \frac{2}{945} + \frac{1}{120} \right) \Lambda^2 + \frac{2}{9,072} \Lambda^3 \right]$$

$$\lambda = \left( \frac{37}{315} - \frac{\Lambda}{945} - \frac{\Lambda^2}{9,072} \right)^2 \Lambda$$

$$\lambda \wedge H(\lambda) = f(\lambda)$$

$$H(\lambda) = .47 - 6\lambda$$

$$\nabla \cdot \lambda = .47 - 6\lambda$$

$$= .47 - 6z \nabla \cdot \lambda$$

$$\nabla \cdot \lambda + 6z \frac{d\lambda}{dx} = .47$$

$$\frac{d}{dx} \left( \nabla \cdot \lambda \right) = \frac{1}{dx} \left[ \nabla \cdot \frac{d\lambda}{dx} + 6z \nabla^2 \lambda \right]$$

$$= \nabla^2 \lambda + 6z \nabla^2 \lambda$$

$$\lambda(2\lambda^2) = .47 \nabla^2 \lambda$$

$$2\lambda^2 = .45 \int \nabla^2 \lambda dx$$

$$\tilde{z} = \frac{\Theta^2}{\lambda} = \frac{.45}{2\lambda} \int \nabla^2 \lambda dx \quad \text{i.e. } \Theta^2(x) = \frac{.47}{2\lambda(x)^2} \int \nabla^2 \lambda(x)^2 dx$$

where  $\nabla^2 \lambda$  potential flow solution geometry  
of interest.

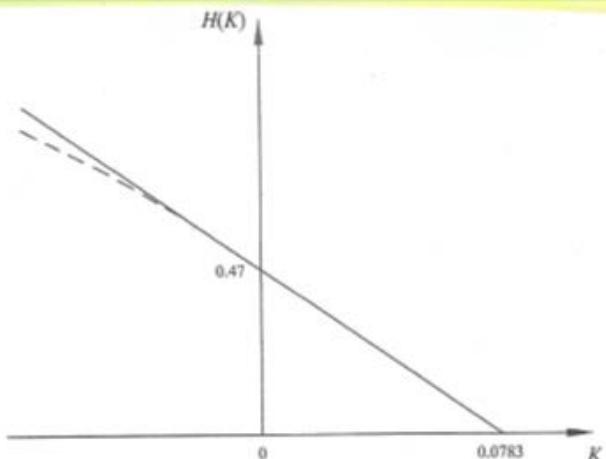


FIGURE 9.7 Exact form of the function  $H(K)$  (solid line) and straight-line approximation (dashed line).

Solution procedure:

$$1. \bar{v}(x)$$

$$2. \Theta(x)$$

$$3. \bar{r}_c(x) \text{ from } \underbrace{\left(\frac{37}{315} - \frac{r_c}{945} - \frac{r_c^2}{9075}\right)^2}_{\Theta^2/\delta^2} r_c = \frac{\Theta^2}{\nu} v_x \text{ note } \bar{r}_c(x) = -\frac{\delta^2}{\nu} v_x$$

$$4. \delta(x) = \Theta(x)$$

$$\frac{\left(\frac{37}{315} - \frac{r_c}{945} - \frac{r_c^2}{9075}\right)}{\Theta(x)}$$

$$\leq \delta^*(x) = \delta \left( \frac{3}{10} - \frac{r_c}{120} \right)$$

$$6. \bar{w}/\nu = f(\gamma) \quad \gamma = \bar{w}/\delta(x)$$

$$7. \bar{z}_0 = \mu \bar{v} \left( 2 + \frac{r_c}{\delta(x)} \right)$$

Inverse problem: for specified  $\bar{r}_c(x) \Rightarrow \bar{v}(x) \Rightarrow$  type II geometry

Example: flat surface ie  $\bar{v} = \text{constant}$ ,  $v_x = 0$  ②

$$② \quad \Theta^2 = .47 \frac{v_x}{\nu} \quad \Theta/x = \frac{.686}{\sqrt{r_c}} \quad r_c = \bar{v}x/\nu$$

$$③ \quad \bar{r}_c = 0$$

$$④ \quad \delta = \frac{315}{37} \Theta \Rightarrow \frac{\delta}{x} = \frac{5.84}{\sqrt{r_c}} \quad \delta^{-1} = \frac{\sqrt{\nu x/\bar{v}}}{5.84 x}$$

$$⑤ \quad \delta^1 = \frac{3}{10} \bar{v} \Rightarrow \frac{\delta^1}{x} = 1.75 / \sqrt{r_c}$$

$$⑥ \quad \bar{z}_0 = \mu \bar{v} z / \delta(x) \Rightarrow \bar{z}_0 / \frac{1}{2} \bar{v} \bar{v}^2 = .686 / \sqrt{r_c}$$

$$\bar{z}_0 / \frac{1}{2} \bar{v} \bar{v}^2 = \frac{2 \mu \bar{v}}{\frac{1}{2} \bar{v} \bar{v}^2} \quad \delta^{-1} = \frac{4 \bar{v}}{\nu} \frac{\bar{v}^{1/2} x^{1/2}}{5.84 x \sqrt{r_c}}$$

$$\bar{z}_0 \text{ within } 3\% \text{ Brems} \quad = .686 \frac{\sqrt{r_c}}{\bar{v}^{1/2} x^{1/2}} \quad = .686 / \sqrt{r_c}$$

ie .686 vs. .686,

whereas using 2nd order

polynomial value was .73

Alternative derivation momentum integral equation #2

$\bar{u} = \text{middle BL where } u = u_x, u_{xy}, \text{ etc.} = 0$

$$\int_0^h [2u_x + u_{yy}] = u_c u_x + \frac{1}{2} u_{yy}$$

$$\int_0^h [u_x - u_c u_x + u_{yy}] = \frac{1}{2} u_{yy} \Big|_0^h = -I_0/\rho$$

$$w = \int_0^y u_y dy = - \int_0^y u_x dy$$

$$\int_0^y u_{yy} dy = \int_0^y \left( - \int_0^x u_x dy \right) u_y dy$$

$$= -u_c \underbrace{\int_0^y u_x dy}_0 + \underbrace{\int_0^y u_{yy} dy}_{w_z \Big|_0^h - \int_0^h z dw}$$

$$\begin{aligned} \text{Integration by parts} \\ \int_0^y w dz &= wz \Big|_0^y - \int_0^y z dw \\ w &= - \int_0^y u_x dy \quad dw = -u_x dy \\ dz &= u_y dy \quad z = y \end{aligned}$$

$$\int_0^h [u_x - u_c u_x - u_c u_x + u_{yy}] dy = -I_0/\rho$$

$$+ u_c - u_{yy} - \int_0^h [u(u_c - u_x) + (u_c - u)u_x] dy - \int_0^h (u_c - u)u_x dy = -I_0/\rho$$

$$\text{or } \underbrace{\frac{du}{dx} \left[ u_c \int_0^y \left( 1 - \frac{u}{u_c} \right) dy \right]}_0 + u_c u_{yy} \underbrace{\int_0^y \left( 1 - \frac{u}{u_c} \right) dy}_{\delta^*} = I_0/\rho$$

$$\frac{du}{dx} [u(u_c - u)] = u_x (u_c - u) + u(u_c - u_x)$$

$$\frac{du}{dx} (u_c^2 \delta) + u_c u_{yy} \delta^* = I_0/\rho$$

Karman-Pohlhausen: Panton

$$u^+ = u/u_e = a + b\gamma + c\gamma^2 + d\gamma^3 \quad \gamma = \frac{y}{\delta}(x)$$

$$u=0 \quad -u_{e\max} = u_{yy} \quad u_{yy} = 0 \quad \gamma = 0$$

$$u=u_e \quad u_y=0 \quad u_{yy}=0 \quad \gamma=\delta$$

$$\frac{\partial u}{\partial y} = 0$$

$$n \geq 2 \text{ for } u/u_e$$

Example: Blasius Bl  $u_e = u_0$

polynomial > 4<sup>th</sup> order

$$u^+ = \frac{3}{2}\gamma - \frac{1}{2}\gamma^3$$

$$\delta^* = \delta \int_0^1 (1-u^+)^2 dy = \frac{3}{8}\delta \quad \Theta = \delta \int_0^1 u^+ (1-u^+)^2 dy = \frac{11}{840} \delta$$

$$T_0/c = \sqrt{u_{yy}} \Big|_{\gamma=0} = \sqrt{\frac{3}{2}} \frac{u_0}{\delta}$$

$$u_e^2 \delta_x = T_0/c \quad u_e \frac{11}{840} \delta_x = \frac{3}{2} \frac{\sqrt{u_0}}{\delta} \Rightarrow \delta = \sqrt{\frac{840}{39}} \sqrt{\frac{u_0}{u_e}} = 4.64 \sqrt{\frac{u_0}{u_e}}$$

$$\frac{u_e^2 m}{840} \int d\delta = \frac{3}{2} \sqrt{u_0} dx$$

$\approx 4.9$  exact value

$$u_e^2 \frac{m}{840} \frac{1}{2} \delta^2 = \frac{3}{2} \sqrt{u_0} x$$

$$\delta^2 = \frac{3 \times 840 \sqrt{x}}{m u_e}$$

$$\delta = 4.64 \sqrt{\frac{\sqrt{x}}{u_e}}$$

### Alternative derivation momentum integral equation #3

Kunden

$$uu_x + uu_y = u_c u_{ex} + \frac{1}{\rho} I_y$$

$$u(u_x + uu_y) + uu_x + uu_y = (u^2)_x + (uu)_y = u_c u_{ex} + \frac{1}{\rho} I_y$$

$$2uu_x + u_y u_x + uu_y$$

$$\int_0^\infty [ (u^2)_x + (uu)_y - u_c u_{ex} ] dy = \frac{1}{\rho} \int_0^\infty I_y dy$$

$$\int_0^\infty [ (u^2)_x - u_c u_{ex} ] dy + u_c v_\infty = -I_w/c$$

$$\int_0^\infty (u_x + uu_y) dy = 0 \quad \int_0^\infty u_x dy = - \int_0^\infty uu_y dy = -v_\infty \Big|_0^\infty = -v_\infty$$

$$\int_0^\infty [ (u^2)_x - u_c u_{ex} - u_c u_x ] dy = -I_w/c$$

$$u_c \int_0^\infty u_x dy = u_c \frac{1}{\Delta x} \int_0^\infty u dy = \frac{1}{\Delta x} \left[ u_c \int_0^\infty u dy \right] - u_{ex} \int_0^\infty u dy$$

$$\frac{1}{\Delta x} \int_0^\infty [ u^2 - u_c u ] dy + u_{ex} \int_0^\infty (u - u_c) dy = -I_w/c$$

$$I_w/c = \underbrace{\frac{1}{\Delta x} u_c^2 \int_0^\infty \left( 1 - \frac{u}{u_c} \right) dy}_0 + u_{ex} \int_0^\infty \left( 1 - \frac{u}{u_c} \right) dy$$

$$I_w/c = \frac{1}{\Delta x} (u_c^2 \sigma) + u_{ex} \delta^*$$

Note  $u_c$  and  $u_{ex}$   $f(x)$

only

Single ODE relates unknowns  $\sigma$ ,  $\delta^*$ ,  $-I_w$

Example Momentum integral  $\sigma_e(x) = (v_0/L)x$   
 merely flow is stagnation point flow  $F_k$  with  $m=1$

$$\delta(x) = \sqrt{v_x/v_e} = [v_L/v_0]^{1/2} = \text{constant}$$

$$\Theta = \int_0^{\infty} \left( 1 - \frac{u}{v_e} \right) dy = \delta \int_0^{\infty} f'(1-f) dy$$

$$= \delta \times \text{constant}$$

$$\begin{aligned} \gamma(x) &= \left[ \frac{1-v_x}{v_0} \right]^{1/2} \\ &= \left[ \frac{v}{v_0} \right]^{1/2} \\ &= \left[ \frac{v_L}{v_0} \right]^{1/2} \end{aligned}$$

$$u/v_e = f'(y)$$

$$\delta^* = \delta \times \text{constant}$$

$$\sin \theta \propto \delta^*$$

$$\gamma = y/\delta$$

integrate velocity  
profile  $\int_0^{\infty} dx \delta$

$$\gamma = [v_x \sigma_e(x)]^{1/2} f(\gamma)$$

$$u = x \gamma = \frac{[v_x \frac{v_0}{L} x]^{1/2} f(\gamma)}{[v_L/v_0]^{1/2}}$$

$$= \frac{v_0}{L} x f'(\gamma)$$

$$= \sigma_e f'(\gamma)$$

$$\begin{aligned} \frac{I_w}{\sigma_e} &= \frac{1}{2x} \left[ \frac{v_0^2 x^2}{L} \Theta \right] + \frac{v_0 x}{L} \delta \int \frac{1}{2x} \left[ \frac{v_0 x}{L} \right] \\ &= \frac{2v_0^2 x}{L^2} \Theta + \frac{v_0^2 x}{L^2} \delta^* \end{aligned}$$

$$\frac{I_w}{\frac{1}{2} v_0^2} = \left( \frac{4\Theta + 2\delta^*}{L} \right) \frac{x}{L} = ax \quad \text{ie linear}$$

linear

one equation three  
unknowns:  $I_w, \Theta, \delta^*$

Can use Newton's method to solve  
(or Karmen-Pohlhausen)

### EXAMPLE 10.6

Use Thwaites' method to estimate the momentum thickness, displacement thickness, and shear stress of the Blasius boundary layer with  $\theta_0 = 0$  at  $x = 0$ .

#### Solution

The solution plan is to use (10.50) to obtain  $\theta$ . Then, because  $dU_e/dx = 0$  for the Blasius boundary layer,  $\lambda = 0$  at all downstream locations and the remaining boundary-layer parameters can be determined from the  $\theta$  results, (10.45), (10.46), and Table 10.2. The first step is setting  $U_e = U =$  constant in (10.50) with  $\theta_0 = 0$ :

$$\theta^2 = \frac{0.45\nu}{U^6} \int_0^x U^5 dx = \frac{0.45\nu}{U} x, \quad \text{or} \quad \theta = 0.671 \sqrt{\frac{\nu x}{U}}$$

This approximate answer is 1% higher than the Blasius-solution value. For  $\lambda = 0$ , the shape factor is  $H(0) = 2.61$ , so:

$$\delta^* = \theta \left( \frac{\delta^*}{\theta} \right) = \theta H(0) = 0.671 \sqrt{\frac{\nu x}{U}} (2.61) = 1.75 \sqrt{\frac{\nu x}{U}}$$

This approximate answer is also 1% higher than the Blasius-solution value. For  $\lambda = 0$ , the skin friction correlation value is  $l(0) = 0.220$ , so:

$$\tau_w = \mu \frac{U}{\theta} l(0) = \frac{\mu U}{0.671 \sqrt{\nu x / U}} (0.220) = \frac{1}{2} \rho U^2 (0.656) \sqrt{\frac{\nu}{U x}}$$

which implies a skin friction coefficient of:

$$C_f = \frac{\tau_w}{\frac{1}{2} \rho U^2} = \frac{0.656}{\sqrt{\text{Re}_x}}$$

which is 1.2% below the Blasius-solution value.

Note: Some Karman-Pohlhausen

$$\text{since we very } H(K) = .47 - 6K \quad K = \frac{\theta^2}{\nu} U_x$$

$$\text{similar or } F(\lambda) = .45 - 6\lambda \quad \lambda = K$$

correlations

Example: Kunder

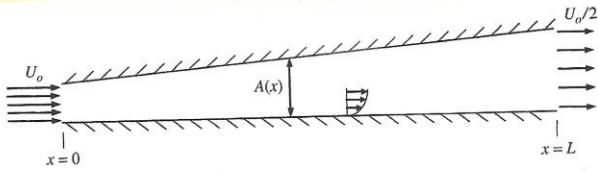


FIGURE 10.10 A simple two-dimensional diffuser of length  $L$  intended to slow the incoming flow to half its speed by doubling the flow area. The resulting adverse pressure gradient in the diffuser influences the character of the boundary layers that develop on the diffuser's inner surfaces, especially when these boundary layers are laminar.

Assume outer flow uniform:  $\tau_{\text{ext}} = \tau_{\text{ext}}(x) A(x)$

$$\Theta^2 = \frac{45\nu}{U_o^2} \int_0^x \tau_{\text{ext}}^2 dx = \frac{45\nu}{U_o^2} (1+x/L)^6 \int_0^x (1+\frac{x}{L})^{-5} dx \quad \tau_{\text{ext}}(x) = \tau_{\text{ext}} (1+x/L)^{-1}$$

$$= \frac{45\nu}{U_o^2} (1+\frac{x}{L})^6 \left[ 1 - (1+\frac{x}{L})^{-4} \right] \frac{L}{4}$$

$$\lambda = \frac{\Theta^2}{2} \tau_{\text{ext}} = \Theta^2 \times \frac{\tau_{\text{ext}}}{\nu} \quad \frac{\tau_{\text{ext}}}{\nu} = -\left(\frac{U_o}{UL}\right) \left(1+\frac{x}{L}\right)^{-2}$$

$$= -\frac{45}{4} \left[ \left(1+\frac{x}{L}\right)^4 - 1 \right]$$

$x/L$	$\lambda$
0	0
0.05	-0.02424
0.10	-0.05221
0.15	-0.08426
0.20	-0.12078

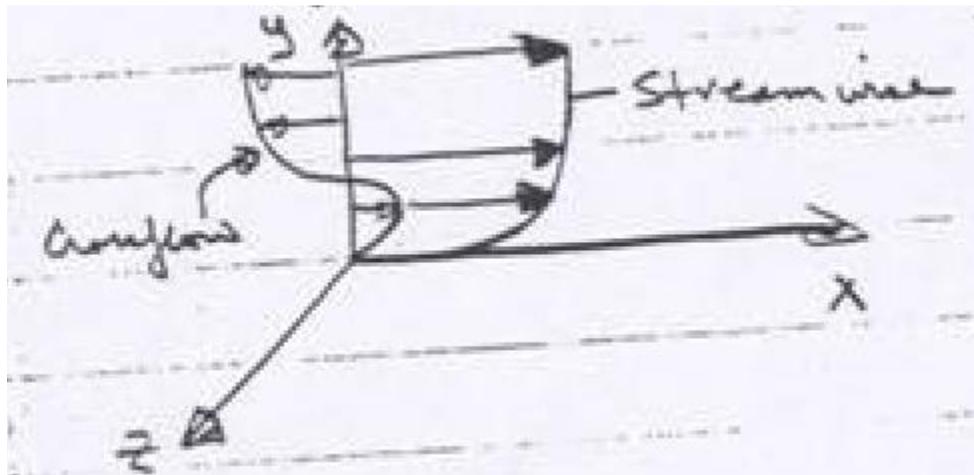
$$\Rightarrow \frac{x}{L} = 0.16 \quad L < L$$

$$\lambda = -0.09$$

$x < \text{separation}$

### 3-D Integral methods

Momentum integral methods perform well (i.e. compare well with experimental data) for a large class of both laminar and turbulent 2D flows. However, for **3D flows they do not**, primarily due to the inability of correlating the crossflow velocity components.



The cross flow is driven by  $\frac{\partial p}{\partial z}$ , which is imposed on BL from the outer potential flow  $U(x,z)$ .

3-D boundary layer equations

$$u_x + v_y + w_z = 0;$$

$$uu_x + vu_y + wu_z = -\frac{\partial}{\partial x}(p/\rho) + vu_{yy} - \frac{\partial}{\partial y}(\bar{u}'v')$$

$$uw_x + vw_y + ww_z = -\frac{\partial}{\partial z}(p/\rho) + vw_{yy} - \frac{\partial}{\partial y}(\bar{v}'w')$$

+ closure equations

Differential methods have been developed for this reason as well as for extensions to more complex and non-thin boundary layer flows.