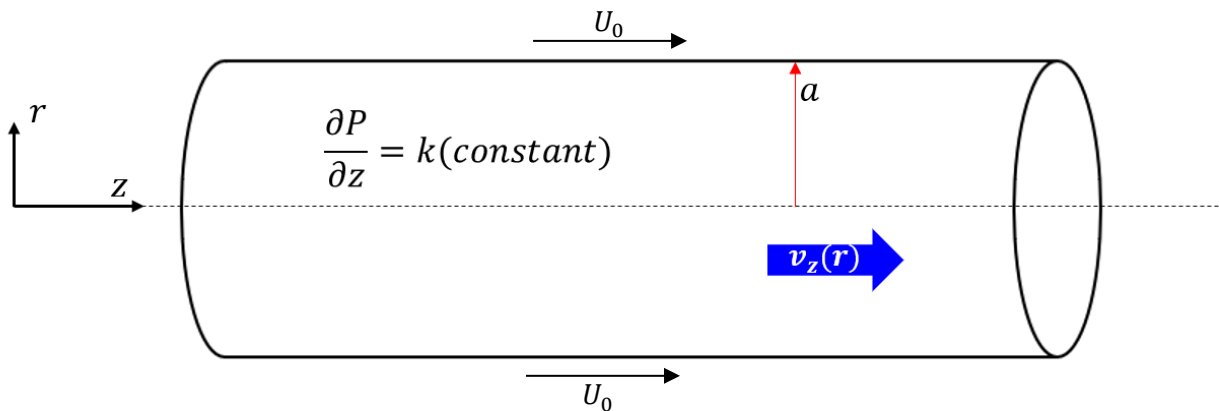


The exam is closed book and closed notes.

The viscous oil in below Figure is set into steady motion by a constant pressure gradient $\frac{\partial P}{\partial z}$. The pipe radius is a and the pipe moves with constant velocity U_0 . Assuming fully developed flow, constant density, circumferentially symmetric flow, and a purely axial fluid motion: (a) Simplify the governing equations (continuity and momentum) with these given conditions. (b) Apply appropriate boundary condition and derive the fluid velocity distribution $v_z(r)$. (c) Calculate wall shear stress at pipe wall.



The equations of motion of an incompressible Newtonian fluid with constant density and viscosity in cylindrical coordinates (r, θ, z) with velocity components (v_r, v_θ, v_z) :

Continuity:

$$\frac{1}{r} \frac{\partial}{\partial r}(r v_r) + \frac{1}{r} \frac{\partial}{\partial \theta}(v_\theta) + \frac{\partial}{\partial z}(v_z) = 0$$

r-momentum:

$$\rho \left(\frac{\partial v_r}{\partial t} + v_r \frac{\partial v_r}{\partial r} + \frac{v_\theta}{r} \frac{\partial v_r}{\partial \theta} + v_z \frac{\partial v_r}{\partial z} - \frac{v_\theta^2}{r} \right) = \rho g_r - \frac{\partial p}{\partial r} + \mu \left[\frac{\partial}{\partial r} \left(\frac{1}{r} \frac{\partial}{\partial r}(r v_r) \right) + \frac{1}{r^2} \frac{\partial^2 v_r}{\partial \theta^2} + \frac{\partial^2 v_r}{\partial z^2} - \frac{2}{r^2} \frac{\partial v_\theta}{\partial \theta} \right]$$

θ -momentum:

$$\rho \left(\frac{\partial v_\theta}{\partial t} + v_r \frac{\partial v_\theta}{\partial r} + \frac{v_\theta}{r} \frac{\partial v_\theta}{\partial \theta} + v_z \frac{\partial v_\theta}{\partial z} + \frac{v_r v_\theta}{r} \right) = \rho g_\theta - \frac{1}{r} \frac{\partial p}{\partial \theta} + \mu \left[\frac{\partial}{\partial r} \left(\frac{1}{r} \frac{\partial}{\partial r}(r v_\theta) \right) + \frac{1}{r^2} \frac{\partial^2 v_\theta}{\partial \theta^2} + \frac{\partial^2 v_\theta}{\partial z^2} + \frac{2}{r^2} \frac{\partial v_r}{\partial \theta} \right]$$

z-momentum:

$$\rho \left(\frac{\partial v_z}{\partial t} + v_r \frac{\partial v_z}{\partial r} + \frac{v_\theta}{r} \frac{\partial v_z}{\partial \theta} + v_z \frac{\partial v_z}{\partial z} \right) = \rho g_z - \frac{\partial p}{\partial z} + \mu \left[\frac{1}{r} \frac{\partial}{\partial r} \left(r \frac{\partial v_z}{\partial r} \right) + \frac{1}{r^2} \frac{\partial^2 v_z}{\partial \theta^2} + \frac{\partial^2 v_z}{\partial z^2} \right]$$

Boundary condition Hint

- At the pipe wall, the velocity is U_0
- At the pipe center, the velocity gradient should be zero

Wall shear stress Hint

- $\tau_{wall} = \mu \frac{\partial v_z}{\partial y} \Big|_{y=0} = -\mu \frac{\partial v_z}{\partial r} \Big|_{r=a}$, $y = a - r$ where a : Radius of pipe

Solution:

ASSUMPTIONS:

1. Steady flow ($\frac{\partial}{\partial t}=0$)
2. Incompressible flow ($\rho=\text{constant}$)
3. Purely axial flow ($v_r=v_\theta=0$) (+3)
4. Circumferentially symmetric flow, so properties do not vary with θ ($\frac{\partial}{\partial \theta}=0$)
5. Constant pressure gradient ($\frac{\partial p}{\partial z}=k$)
6. Horizontal cylinders ($g_z=0$)

(a)

Continuity:

$$\frac{1}{r} \frac{\partial}{\partial r} (r v_r) + \frac{1}{r} \frac{\partial}{\partial \theta} (v_\theta) + \frac{\partial}{\partial z} (v_z) = 0$$

$$0(3) + 0(3) + \frac{\partial v_z}{\partial z} = 0 \quad (+1)$$

z-momentum:

$$\rho \left(\frac{\partial v_z}{\partial t} + v_r \frac{\partial v_z}{\partial r} + \frac{v_\theta}{r} \frac{\partial v_z}{\partial \theta} + v_z \frac{\partial v_z}{\partial z} \right) = \rho g_z - \frac{\partial p}{\partial z} + \mu \left[\frac{1}{r} \frac{\partial}{\partial r} \left(r \frac{\partial v_z}{\partial r} \right) + \frac{1}{r^2} \frac{\partial^2 v_z}{\partial \theta^2} + \frac{\partial^2 v_z}{\partial z^2} \right] \quad (+1.5)$$

$$\rho(0(1) + 0(3) + 0(3,4) + 0(\text{continuity})) = 0(6) - k(5) + \mu \left[\frac{1}{r} \frac{\partial}{\partial r} \left(r \frac{\partial v_z}{\partial r} \right) + 0(4) + 0(\text{continuity}) \right]$$

$$\frac{\mu}{r} \frac{\partial}{\partial r} \left(r \frac{\partial v_z}{\partial r} \right) = k \quad (+1)$$

(b) Integrate

$$\frac{\partial}{\partial r} \left(r \frac{\partial v_z}{\partial r} \right) = \frac{k}{\mu} r$$

$$r \frac{\partial v_z}{\partial r} = \frac{k}{2\mu} r^2 + C_1$$

$$\frac{\partial v_z}{\partial r} = \frac{k}{2\mu} r + \frac{C_1}{r}$$

$$\therefore v_z(r) = \frac{k}{4\mu} r^2 + C_1 \ln(r) + C_2 \quad (+1)$$

Apply two boundary conditions

$$v_z(a) = U_0 \rightarrow \frac{k}{4\mu} a^2 + C_1 \ln(a) + C_2 = U_0 \quad (+0.5)$$

$$\left. \frac{\partial v_z}{\partial r} \right|_{r=0} = 0 \rightarrow \frac{k}{2\mu} (0) + \frac{C_1}{(0)} = 0 \quad (+0.5)$$

$$\therefore C_1 = 0$$

$$\therefore C_2 = U_0 - \frac{k}{4\mu} a^2$$

Hence,

$$\therefore v_z(r) = U_0 + \frac{k}{4\mu} r^2 - \frac{k}{4\mu} a^2 = U_0 + \frac{k}{4\mu} (r^2 - a^2) = U_0 + \frac{1}{4\mu} \frac{\partial P}{\partial z} (r^2 - a^2) \quad (+1)$$

(c) Wall shear stress at the pipe wall

$$\tau_{wall} = -\mu \left. \frac{\partial v_z}{\partial r} \right|_{r=a}$$

$$\mu \frac{\partial v_z}{\partial r} = -\frac{k}{2} r$$

Apply

$$r = a$$

$$\therefore \tau_{wall} = -\frac{ka}{2} = -\frac{a}{2} \frac{\partial P}{\partial z} \quad (+0.5)$$