

**The exam is closed book and closed notes.**

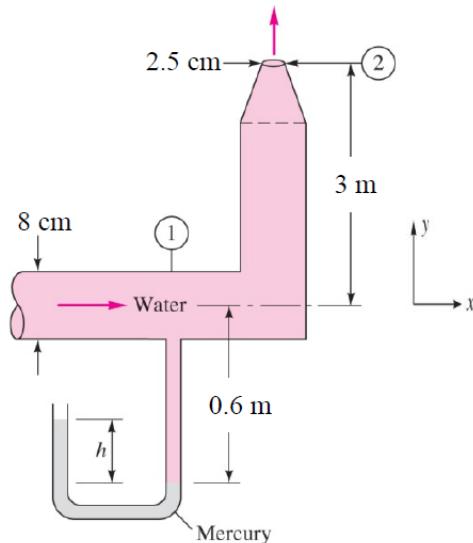
1. In the Figure below the bend is flanged at section 1 (the flange is not shown) and the flow exits to atmosphere at section 2. If  $V_1 = 0.5 \text{ m/s}$ ,  $h = 40 \text{ cm}$ ,  $\rho_{\text{water}} = 998 \text{ kg/m}^3$ , and  $\rho_{\text{mercury}} = 13,550 \text{ kg/m}^3$ , neglecting the gravity forces and assuming uniform flows at 1 and 2, find: a)  $V_2$  using continuity equation; b)  $p_1$  using manometry equation; c) the force components on the flange bolts in  $x$  and  $y$  directions using linear momentum equations; d) the friction head loss between 1 and 2 using energy equation.

$$\text{Continuity equation: } -\frac{d}{dt} \int_{CV} \rho dV = \int_{CS} \rho \underline{V}_R \cdot \underline{n} dA$$

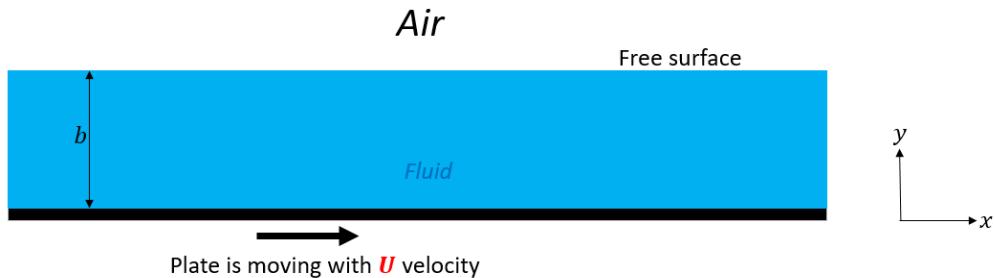
$$\text{Momentum equation: } \sum F = \frac{d}{dt} \int_{CV} \rho \underline{V} dV + \int_{CS} \rho \underline{V} \underline{V}_R \cdot \underline{n} dA$$

**Energy Equation (for incompressible steady flow):**

$$\left( \frac{p}{\rho g} + \frac{\alpha V^2}{2g} + z \right)_1 = \left( \frac{p}{\rho g} + \frac{\alpha V^2}{2g} + z \right)_2 + h_{\text{turbine}} - h_{\text{pump}} + h_{\text{friction}}$$



2. The viscous, incompressible flow between the parallel plates shown in Figure is caused by the motion of the bottom plate. Assuming pressure gradient along the  $x$  direction is constant ( $\frac{\partial P}{\partial x} = C$ ), steady, 2D, and parallel flow and using differential analysis: (a) Show that the flow is fully developed using continuity equation; (b) Find the velocity profile  $u(y)$  using Navier-Stokes equations with appropriate boundary conditions; (c) Find wall shear stress at bottom wall; and (d) Find the flow rate (hint:  $Q = \int \underline{V} \cdot \underline{n} dA$  and assume constant width w). **Explicitly state all assumptions.**



#### Incompressible Continuity Equation:

$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} + \frac{\partial w}{\partial z} = 0$$

#### Incompressible Navier-Stokes Equations in Cartesian Coordinates:

$$\rho g_x - \frac{\partial p}{\partial x} + \mu \left( \frac{\partial^2 u}{\partial x^2} + \frac{\partial^2 u}{\partial y^2} + \frac{\partial^2 u}{\partial z^2} \right) = \rho \left( \frac{\partial u}{\partial t} + u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} + w \frac{\partial u}{\partial z} \right)$$

$$\rho g_y - \frac{\partial p}{\partial y} + \mu \left( \frac{\partial^2 v}{\partial x^2} + \frac{\partial^2 v}{\partial y^2} + \frac{\partial^2 v}{\partial z^2} \right) = \rho \left( \frac{\partial v}{\partial t} + u \frac{\partial v}{\partial x} + v \frac{\partial v}{\partial y} + w \frac{\partial v}{\partial z} \right)$$

$$\rho g_z - \frac{\partial p}{\partial z} + \mu \left( \frac{\partial^2 w}{\partial x^2} + \frac{\partial^2 w}{\partial y^2} + \frac{\partial^2 w}{\partial z^2} \right) = \rho \left( \frac{\partial w}{\partial t} + u \frac{\partial w}{\partial x} + v \frac{\partial w}{\partial y} + w \frac{\partial w}{\partial z} \right)$$

**Shear stress** (At free surface, shear stress is zero)

$$\tau_{xy} = \tau_{yx} = \mu \left( \frac{\partial u}{\partial y} + \frac{\partial v}{\partial x} \right)$$

3. The power  $P$  developed by a wind turbine is a function of turbine's diameter  $D$ , air density  $\rho$ , wind speed  $V$ , and rotation rate  $\omega$ . Namely it can be written as  $P = f(D, \rho, V, \omega)$ . Viscosity effects are negligible. Rewrite this relationship in dimensionless form.

Quantity	Symbol	Dimensions	
		$MLT\Theta$	$FLT\Theta$
Length	$L$	$L$	$L$
Area	$A$	$L^2$	$L^2$
Volume	$V$	$L^3$	$L^3$
Velocity	$V$	$LT^{-1}$	$LT^{-1}$
Acceleration	$dV/dt$	$LT^{-2}$	$LT^{-2}$
Speed of sound	$a$	$LT^{-1}$	$LT^{-1}$
Volume flow	$Q$	$L^3T^{-1}$	$L^3T^{-1}$
Mass flow	$\dot{m}$	$MT^{-1}$	$FTL^{-1}$
Pressure, stress	$p, \sigma, \tau$	$ML^{-1}T^{-2}$	$FL^{-2}$
Strain rate	$\dot{\epsilon}$	$T^{-1}$	$T^{-1}$
Angle	$\theta$	None	None
Angular velocity	$\omega, \Omega$	$T^{-1}$	$T^{-1}$
Viscosity	$\mu$	$ML^{-1}T^{-1}$	$FTL^{-2}$
Kinematic viscosity	$\nu$	$L^2T^{-1}$	$L^2T^{-1}$
Surface tension	$\gamma$	$MT^{-2}$	$FL^{-1}$
Force	$F$	$MLT^{-2}$	$F$
Moment, torque	$M$	$ML^2T^{-2}$	$FL$
Power	$P$	$ML^2T^{-3}$	$FLT^{-1}$
Work, energy	$W, E$	$ML^2T^{-2}$	$FL$
Density	$\rho$	$ML^{-3}$	$FT^2L^{-4}$
Temperature	$T$	$\Theta$	$\Theta$
Specific heat	$c_p, c_v$	$L^2T^{-2}\Theta^{-1}$	$L^2T^{-2}\Theta^{-1}$
Specific weight	$\gamma$	$ML^{-2}T^{-2}$	$FL^{-3}$
Thermal conductivity	$k$	$MLT^{-3}\Theta^{-1}$	$FT^{-1}\Theta^{-1}$
Thermal expansion coefficient	$\beta$	$\Theta^{-1}$	$\Theta^{-1}$

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Exam 1

Time: 50 minutes

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**Solution 1:**

a) Continuity:

$$A_1 V_1 = A_2 V_2$$

$$V_2 = \frac{A_1 V_1}{A_2} = \frac{(\pi/4)D_1^2 V_1}{(\pi/4)D_2^2} = \frac{D_1^2 V_1}{D_2^2} = \frac{(0.08)^2(0.5)}{(0.025)^2} = 5.12 \text{ m/s}$$

+3.5

b) Manometry:

$$p_1 + \rho_{water} g(0.6) - \rho_{mercury} gh = p_a = 0$$

$$p_1 = \rho_{mercury} gh - \rho_{water} g(0.6)$$

$$= (13550)(9.81)(0.4) - (998)(9.81)(0.6) = 47,296 \text{ pa (gage)}$$

+3

c)  $x$  – momentum:

$$\sum F_x = \dot{m} u_2 - \dot{m} u_1$$

$$-F_{x,bolts} + p_1 A_1 = \rho Q (0 - V_1)$$

$$F_{x,bolts} = p_1 A_1 + \rho A_1 V_1 (V_1) = A_1 (p_1 + \rho V_1^2)$$

$$F_{x,bolts} = \left[ \frac{\pi}{4} (0.08)^2 \right] [(47296) + (998)(0.5)^2] = 239 \text{ N}$$

+2

 $y$  – momentum:

$$\sum F_y = \dot{m} v_2 - \dot{m} v_1$$

$$-F_{y,bolts} = \rho Q (V_2 - 0)$$

$$F_{y,bolts} = -\rho A_2 V_2^2 = -(998) \left[ \frac{\pi}{4} (0.025)^2 \right] (5.12)^2 = -12.84 \text{ N}$$

+1

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d) Energy equation:

$$\frac{p_1}{\rho g} + \frac{\alpha_1 V_1^2}{2g} + z_1 = \frac{p_2}{\rho g} + \frac{\alpha_2 V_2^2}{2g} + z_2 + h_f$$

$$\frac{(47296)}{(998)(9.81)} + \frac{(1.0)(0.5)^2}{2(9.81)} + 0 = 0 + \frac{(1.0)(5.12)^2}{2(9.81)} + (3.0) + h_f$$

$$h_f = 0.51 \text{ m}$$

+0.5

**Solution 2:**

KNOWN: *Flow condition, Boundary condition*

FIND: (2)

- Show that the flow is fully developed
- velocity profile  $u(y)$
- Find wall shear stress at bottom wall
- Find the flow rate

ASSUMPTIONS:

- steady:  $\frac{\partial}{\partial t} = 0$
- 2D flow:  $w = 0; \frac{\partial}{\partial z} = 0$
- Parallel flow:  $v = w = 0$
- $\frac{\partial p}{\partial x} = \text{constant}$

ANALYSIS:

(a) Continuity

$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} + \frac{\partial w}{\partial z} = 0$$

$$\frac{\partial u}{\partial x} + 0 + 0 = 0 \rightarrow \frac{\partial u}{\partial x} = 0 \rightarrow \text{fully developed} \quad \text{(2)}$$

(b)  $x$ -momentum equation

$$\rho \left( \frac{\partial u}{\partial t} + u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} + w \frac{\partial u}{\partial z} \right) = \rho g_x - \frac{\partial p}{\partial x} + \mu \left( \frac{\partial^2 u}{\partial x^2} + \frac{\partial^2 u}{\partial y^2} + \frac{\partial^2 u}{\partial z^2} \right)$$

$$0 = -\frac{\partial P}{\partial x} + \mu \frac{\partial^2 u}{\partial y^2}$$

$$\frac{\partial^2 u}{\partial y^2} = \frac{1}{\mu} \frac{\partial p}{\partial x} \quad \text{(1.5)}$$

Integrate twice

$$u(y) = \frac{1}{2\mu} \frac{\partial p}{\partial x} y^2 + c_1 y + c_2 \quad \text{(1.5)}$$

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Apply boundary conditions

$$y = 0 \rightarrow u = U \rightarrow c_2 = U$$

$$y = b \rightarrow \tau = 0 \rightarrow \mu \left( \frac{\partial u}{\partial y} \right) = 0 \rightarrow \mu \left( \frac{1}{\mu} \left( \frac{\partial p}{\partial x} \right) b + c_1 \right) = 0 \quad (2)$$

$$c_1 = -\frac{1}{\mu} \left( \frac{\partial p}{\partial x} \right) b$$

Therefore,

$$u(y) = \frac{1}{2\mu} \frac{\partial p}{\partial x} y^2 - \frac{b}{\mu} \left( \frac{\partial p}{\partial x} \right) y + U$$

$$u(y) = \frac{1}{2\mu} \left( \frac{\partial p}{\partial x} \right) (y^2 - 2by) + U$$

(c) Shear stress at bottom wall

$$\tau = \mu \frac{du}{dy} = \mu \left\{ \frac{1}{2\mu} \left( \frac{\partial p}{\partial x} \right) (2y - 2b) \right\} = \left( \frac{\partial p}{\partial x} \right) (y - b)$$

$$\tau_{wall} = \tau(0) = -b \left( \frac{\partial p}{\partial x} \right) \quad (0.5)$$

(d) Flow rate

$$Q = \int \underline{V} \cdot \underline{n} dA = w \int_0^b u(y) dy = \frac{w}{2\mu} \left( \frac{\partial p}{\partial x} \right) \left( \frac{1}{3} y^3 - by^2 \right)_0^b + wU(y)_0^b$$

$$Q = \frac{w}{2\mu} \left( \frac{\partial p}{\partial x} \right) \left( \frac{1}{3} b^3 - b^3 \right) + wUb = -\frac{wb^3}{3\mu} \left( \frac{\partial p}{\partial x} \right) + wUb \quad (0.5)$$

**Solution 3:**

ASSUMPTIONS: the problem is only a function of the above dimensional variables

ANALYSIS:

$$P = f(D, \rho, V, \omega).$$

$$P = \left\{ \frac{ML^2}{T^3} \right\}, \quad D = \{L\}, \quad \rho = \left\{ \frac{M}{L^3} \right\}, \quad V = \left\{ \frac{L}{T} \right\}, \quad \omega = \left\{ \frac{1}{T} \right\}$$

(4)

$$j = 3 \rightarrow k = n - j = 5 - 3 = 2$$

The repeating variables are  $D, \rho, V$

Calculate first non-dimensional group

$$\Pi_0 = PD^a \rho^b V^c$$

$$\text{unit } [\Pi_0] \rightarrow \left\{ \frac{ML^2}{T^3} \right\} \{L^a\} \left\{ \frac{M^b}{L^{3b}} \right\} \left\{ \frac{L^c}{T^c} \right\}$$

(2)

Above one should be non-dimensional

$$\begin{aligned} [M] &\rightarrow 1 + b = 0 \\ [L] &\rightarrow 2 + a - 3b + c = 0 \\ [T] &\rightarrow -3 - c = 0 \\ \therefore b &= -1, c = -3, a = -2 \end{aligned}$$

$$\therefore \Pi_0 = PD^{-2} \rho^{-1} V^{-3} = \frac{P}{\rho D^2 V^3}$$

(1)

Calculate second non-dimensional group

$$\begin{aligned} \Pi_1 &= \omega D^a \rho^b V^c \\ \text{unit } [\Pi_1] &\rightarrow \left\{ \frac{1}{T} \right\} \{L^a\} \left\{ \frac{M^b}{L^{3b}} \right\} \left\{ \frac{L^c}{T^c} \right\} \\ [M] &\rightarrow b = 0 \\ [L] &\rightarrow a - 3b + c = 0 \\ [T] &\rightarrow -1 - c = 0 \\ \therefore b &= 0, c = -1, a = 1 \\ \therefore \Pi_1 &= \omega D^1 \rho^0 V^{-1} = \frac{\omega D}{V} \end{aligned}$$

(2)

As a result,

$$\Pi_0 = fnc(\Pi_1) \rightarrow \frac{P}{\rho D^2 V^3} = fnc \left( \frac{\omega D}{V} \right)$$

(1)